Summary for Subcatchment 3S: Urban Commercial wth Open Space

Runoff

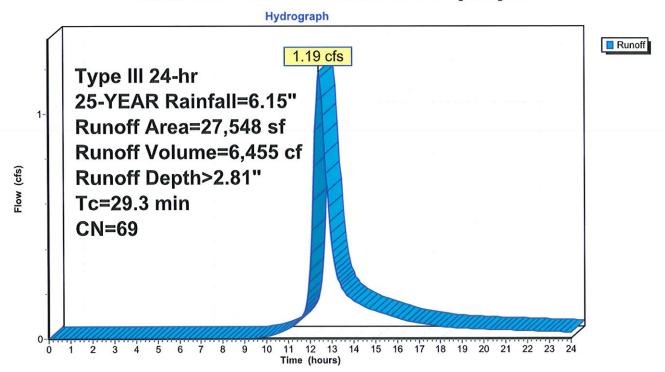
1.19 cfs @ 12.42 hrs, Volume=

6,455 cf, Depth> 2.81"

Runoff by SCS TR-20 method, UH=SCS, Time Span= 0.00-24.00 hrs, dt= 0.05 hrs Type III 24-hr 25-YEAR Rainfall=6.15"

 A	rea (sf)	CN	Description					
	27,548	69	50-75% Grass cover, Fair, HSG B					
1	27,548	8 100.00% Pervious Area			a			
Tc (min)	Length (feet)	Slope (ft/ft	velocity (ft/sec)	Capacity (cfs)	Description			
29.3					Direct Entry, DIRECT			

Subcatchment 3S: Urban Commercial wth Open Space



Hydrograph for Subcatchment 3S: Urban Commercial wth Open Space

Time Precip. Excess Runoff (hours) (inches) (inches) (inches) (cfs) (hours) (inches) (inches) (inches) (cfs) (hours) (inches) (inches) (inches) (cfs) (hours) (inches) (hours) (inches) (hours) (inches) (hours) (inches) (hours) (inches) (hours) (inches) (hours)			-	_			
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	12.75	4.48	1.59	0.73			

POST DEVEL

Prepared by Fuller Engineering & Land Surveying, LLC HydroCAD® 10.00 s/n 02123 © 2011 HydroCAD Software Solutions LLC

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Page 21

Summary for Reach 1R: CONTROL STRUCTURE

Inflow Area = 59,949 sf, 40.15% Impervious, Inflow Depth = 1.17" for 25-YEAR event

Inflow = 1.76 cfs @. 12.87 hrs, Volume = 5.838 cf

Outflow = 1.76 cfs @ 12.87 hrs, Volume= 5,838 cf, Atten= 0%, Lag= 0.0 min

Routing by Stor-Ind+Trans method, Time Span= 0.00-24.00 hrs, dt= 0.05 hrs

Max. Velocity= 154.72 fps, Min. Travel Time= 0.0 min

Avg. Velocity = 154.72 fps, Avg. Travel Time= 0.0 min

Peak Storage= 0 cf @ 12.87 hrs

Average Depth at Peak Storage= 0.01'

Bank-Full Depth= 12.00' Flow Area= 19.6 sf, Capacity= 3,515.86 cfs

Custom stage-perimeter table, n= 0.013 Concrete pipe, bends & connections

100 Intermediate values determined by Multi-point interpolation

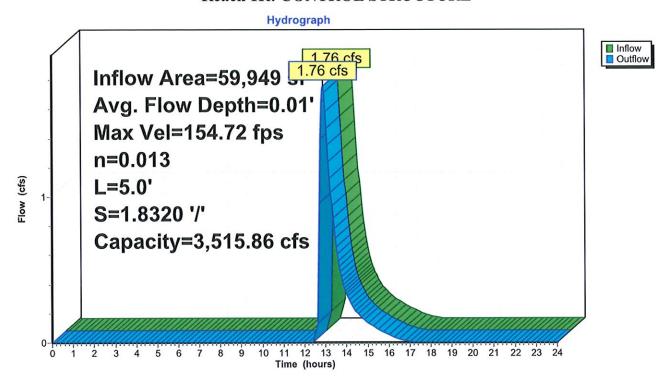
Length= 5.0' Slope= 1.8320 '/'

Inlet Invert= 61.16', Outlet Invert= 52.00'

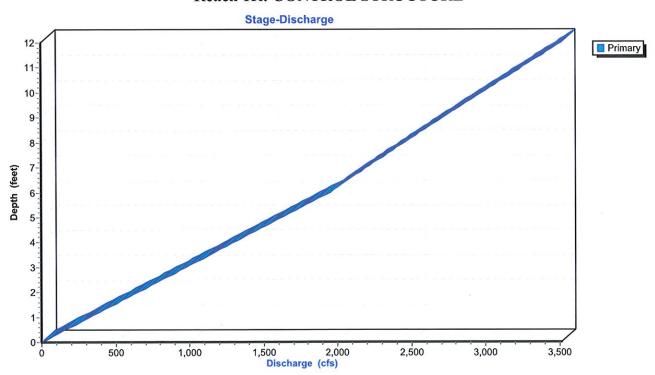


Depth (feet)	End Area (sq-ft)	Perim. (feet)	Storage (cubic-feet)	Discharge (cfs)
0.00	0.0	0.0	0	0.00
6.00	12.6	12.6	63	1,949.43
12.00	19.6	15.7	98	3,515.86

Reach 1R: CONTROL STRUCTURE

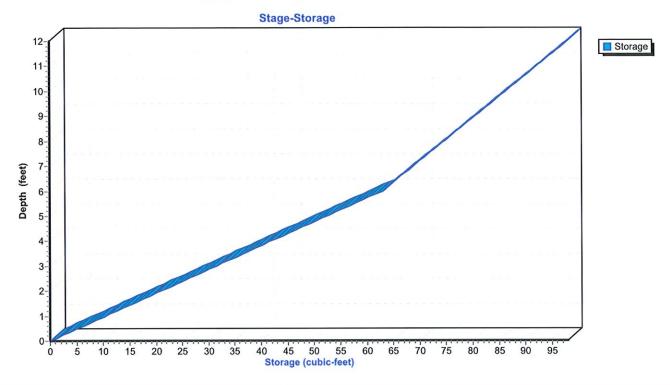


Reach 1R: CONTROL STRUCTURE



Printed 1/24/2022 Page 23

Reach 1R: CONTROL STRUCTURE



Prepared by Fuller Engineering & Land Surveying, LLC HydroCAD® 10.00 s/n 02123 © 2011 HydroCAD Software Solutions LLC

Hydrograph for Reach 1R: CONTROL STRUCTURE

Time	Inflow	Storage	Elevation	Outflow
(hours)	(cfs)	(cubic-feet)	(feet)	(cfs)
0.00	0.00	0	61,16	0.00
0.50	0.00	0	61.16	0.00
1.00	0.00	0	61.16	0.00
1.50	0.00	0	61.16	0.00
2.00	0.00	0	61.16	0.00
2.50	0.00	0	61.16	0.00
3.00	0.00	0	61.16	0.00
3.50	0.00	0	61.16	0.00
4.00	0.00	0	61.16	0.00
4.50	0.00	0	61.16	0.00
5.00	0.00	0	61.16	0.00
5.50	0.00	0	61.16	0.00
6.00	0.00	0	61.16	0.00
6.50	0.00	0	61.16	0.00
7.00	0.00	0	61.16	0.00
7.50	0.00	0	61.16	0.00
8.00	0.00	0	61.16	0.00
8.50	0.00	0	61.16	0.00
9.00	0.00	0	61.16	0.00
9.50	0.00	0	61.16	0.00
10.00	0.00	0	61.16	0.00
10.50	0.00	0	61.16	0.00
11.00	0.00	0	61.16	0.00
11.50	0.00	0	61.16	0.00
12.00	0.00	0	61.16	0.00
12.50	0.00	0	61.16	0.00
13.00	1.59	0	61.16	1.59
13.50	0.66	0	61.16	0.66
14.00	0.34	0	61.16	0.34
14.50	0.21	0	61.16	0.21
15.00	0.14	0	61.16	0.14
15.50	0.09	0	61.16	0.09
16.00	0.06	0	61.16	0.06
16.50	0.02	0	61.16	0.02
17.00	0.00	0	61.16	0.00
17.50	0.00	0	61.16	0.00
18.00	0.00	0	61.16	0.00
18.50	0.00	0	61.16	0.00
19.00	0.00	0	61.16	0.00
19.50	0.00	0	61.16	0.00
20.00	0.00	0	61.16	0.00
20.50	0.00	0	61.16	0.00
21.00	0.00	0	61.16	0.00
21.50	0.00	0	61.16	0.00
22.00	0.00	0	61.16	0.00
22.50	0.00	0	61.16	0.00
23.00	0.00	0	61.16	0.00
23.50	0.00	0	61.16	0.00
24.00	0.00	0	61.16	0.00

Stage-Discharge for Reach 1R: CONTROL STRUCTURE

		_			
Elevation	Velocity	Discharge	Elevation	Velocity	Discharge
(feet)	(ft/sec)	(cfs)	(feet)	(ft/sec)	(cfs)
61.16	0.00	0.00	68.96	163.51	2,403.64
61.31	154.72	48.74	69.11	164.18	2,442.20
61.46	154.72	97.47	69.26	164.84	2,480.87
61.61	154.72	146.21	69.41	165.49	2,519.63
61.76	154.72	194.94	69.56	166.14	2,558.48
61.91	154.72	243.68	69.71	166.77	2,597.44
62.06	154.72	292.42	69.86	167.39	2,636.48
62.21	154.72	341.15	70.01	168.01	2,675.62
62.36	154.72	389.89	70.16	168.62	2,714.84
62.51	154.72	438.62	70.31	169.23	2,754.15
62.66	154.72	487.36	70.46	169.82	2,793.55
62.81	154.72	536.09	70.61	170.41	2,833.04
62.96	154.72	584.83	70.76	170.99	2,872.60
63.11	154.72	633.57	70.91	171.56	2,912.25
63.26	154.72	682.30	71.06	172.13	2,951.98
63.41	154.72	731.04	71.21	172.69	2,991.79
63.56	154.72	779.77	71.36	173.24	3,031.67
63.71	154.72	828.51	71.51	173.78	3,071.63
63.86	154.72	877.25	71.66	174.32	3,111.67
64.01	154.72	925.98	71.81	174.86	3,151.77
64.16	154.72	974.72	71.96	175.38	3,191.95
64.31	154.72	1,023.45	72.11	175.90	3,232.21
64.46	154.72	1,072.19	72.26	176.42	3,272.53
64.61	154.72	1,120.93	72.41	176.92	3,312.92
64.76	154.72	1,169.66	72.56	177.43	3,353.37
64.91	154.72	1,218.40	72.71	177.92	3,393.90
65.06	154.72	1,267.13	72.86	178.41	3,434.50
65.21	154.72	1,315.87	73.01	178.90	3,475.15
65.36	154.72	1,364.60	73.16	179.38	3,515.86
65.51	154.72	1,413.34			
65.66	154.72	1,462.08			
65.81	154.72	1,510.81			
65.96	154.72	1,559.55			
66.11	154.72	1,608.28			
66.26	154.72	1,657.02			
66.41	154.72	1,705.76			
66.56	154.72	1,754.49			
66.71	154.72	1,803.23			
66.86		1,851.96			
67.01	154.72	1,900.70			
67.16		1,949.43			
67.31	155.51	1,986.64			
67.46		2,023.96			
67.61	157.06	2,061.41			
67.76		2,098.97			
67.91	158.56	2,136.67			
68.06		2,174.48			
68.21	160.03	2,212.40			
68.36		2,250.42			
68.51		2,288.57			
68.66		2,326.83			
68.81		2,365.18			

Stage-Area-Storage for Reach 1R: CONTROL STRUCTURE

		Buge Men c	torage for	Iteach II	. COMMODE
	End-Area	Storage		End-Area	Storage
(feet)	(sq-ft)	(cubic-feet)	(feet)	(sq-ft)	(cubic-feet)
61.16	0.0	0	68.96	14.7	74
61.31	0.3	2 3	69.11	14.9	74
61.46	0.6	3	69.26	15.1	75
61.61	0.9	5	69.41	15.2	76
61.76	1.3	6	69.56	15.4	77
61.91	1.6	8	69.71	15.6	78
62.06	1.9	9	69.86	15.8	79
62.21	2.2	11	70.01	15.9	80
62,36	2.5	13	70.16	16.1	81
62.51	2.8	14	70.31	16.3	81
62.66	3.1	16	70.46	16.4	82
62.81	3.5	17	70.61	16.6	83
62.96	3.8	19	70.76	16.8	84
63.11	4.1	20	70.91	17.0	85
63.26	4.4	22	71.06	17.2	86
63.41	4.7	24	71.21	17.3	87
63.56	5.0	25	71.36	17.5	88
63.71	5.4	27	71.51	17.7	88
63.86	5.7	28	71.66	17.9	89
64.01	6.0	30	71.81	18.0	90
64.16	6.3	32	71.96	18.2	91
64.31	6.6	33	72.11	18.4	92
64.46	6.9	35	72.26	18.6	93
64.61	7.2	36	72.41	18.7	94
64.76	7.6	38	72.56	18.9	95
64.91	7.9	39	72.71	19.1	95
65.06	8.2	41	72.86	19.3	96
65.21	8.5	43	73.01	19.4	97
65.36	8.8	44	73.16	19.6	98
65.51	9.1	46			
65.66	9.4	47			
65.81	9.8	49			
65.96	10.1	50			
66.11	10.4	52			
66.26	10.7	54			
66.41	11.0	55			
66.56		57			
66.71	11.7	58			
66.86		60			
67.01		61			
67.16		63			
67.31	12.8	64			
67.46	12.9	65			
67.61		66			
67.76		67			
67.91		67			
68.06		68			
68.21		69			
68.36		70			
68.51		71			
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68.81	14.5	73	ļ		
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POST DEVEL

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Page 27

Summary for Reach 2R: Rip Rap Pool

[62] Hint: Exceeded Reach 1R OUTLET depth by 0.43' @ 12.90 hrs

Inflow Area = 59,949 sf, 40.15% Impervious, Inflow Depth = 1.17" for 25-YEAR event

Inflow = 1.76 cfs @ 12.87 hrs, Volume= 5,838 cf

Outflow = 1.76 cfs @ 12.88 hrs, Volume= 5,838 cf, Atten= 0%, Lag= 0.5 min

Routing by Stor-Ind+Trans method, Time Span= 0.00-24.00 hrs, dt= 0.05 hrs

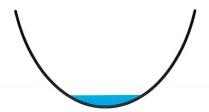
Max. Velocity= 2.45 fps, Min. Travel Time= 0.1 min Avg. Velocity = 1.25 fps, Avg. Travel Time= 0.1 min

Peak Storage= 7 cf @ 12.88 hrs Average Depth at Peak Storage= 0.44' Bank-Full Depth= 3.50' Flow Area= 16.3 sf, Capacity= 130.02 cfs

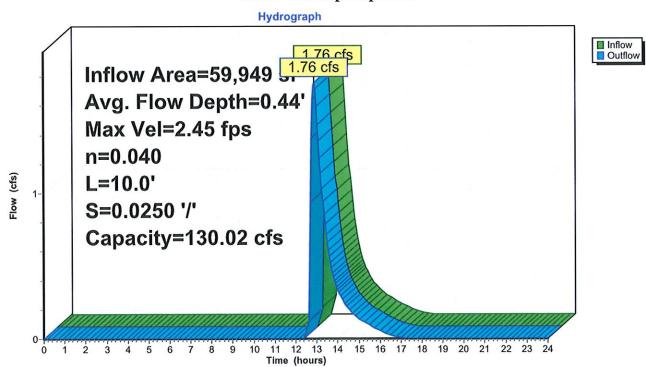
7.00' x 3.50' deep Parabolic Channel, n= 0.040 Earth, cobble bottom, clean sides

Length= 10.0' Slope= 0.0250 '/'

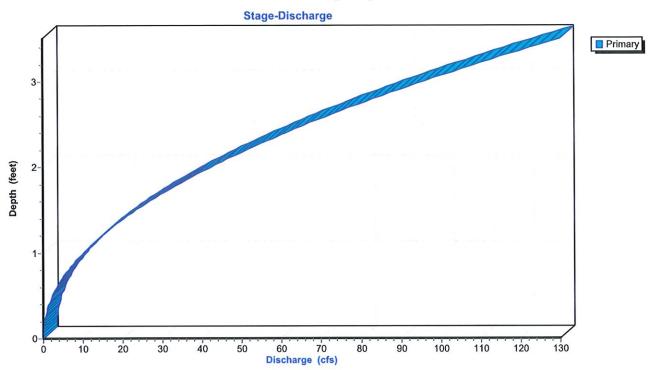
Inlet Invert= 52.00', Outlet Invert= 51.75'



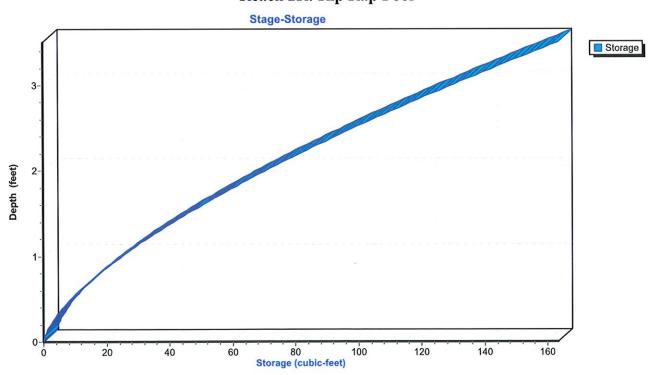
Reach 2R: Rip Rap Pool



Reach 2R: Rip Rap Pool



Reach 2R: Rip Rap Pool



Hydrograph for Reach 2R: Rip Rap Pool

Time	Inflow	Storage	Elevation	Outflow
(hours)	(cfs)	(cubic-feet)	(feet)	(cfs)
0.00	0.00	0	52.00	0.00
0.50	0.00	0	52.00	0.00
1.00	0.00	Ö	52.00	0.00
1.50	0.00	0	52.00	0.00
2.00	0.00	0	52.00	0.00
2.50	0.00	Ö	52.00	0.00
3.00	0.00	0	52.00	0.00
3.50	0.00	0	52.00	0.00
4.00	0.00	0	52.00	0.00
4.50	0.00	0	52.00	0.00
5.00	0.00	0	52.00	0.00
5.50	0.00	0	52.00	0.00
6.00	0.00	0	52,00	0.00
6.50	0.00	0	52.00	0.00
7.00	0.00	0	52.00	0.00
7.50	0.00	0	52.00	0.00
8.00	0.00	0	52,00	0.00
8.50	0.00	0	52.00	0.00
9.00	0.00	0	52.00	0.00
9.50	0.00	ő	52.00	0.00
10.00	0.00	0	52.00	0.00
10.50	0.00	0	52.00	0.00
11.00	0.00	0	52.00	0.00
11.50	0.00	ő	52.00	0.00
12.00	0.00	ŏ	52.00	0.00
12.50	0.00	0	52.00	0.00
13.00	1.59	7	52.42	1.60
13.50	0.66	4	52.28	0.66
14.00	0.34	2	52.20	0.34
14.50	0.21	2	52.16	0.21
15.00	0.14	1	52.13	0.14
15.50	0.09	1	52.11	0.09
16.00	0.06	1	52.08	0.06
16.50	0.02	Ô	52.05	0.02
17.00	0.00	0	52.02	0.00
17.50	0.00	0	52.00	0.00
18.00	0.00	0	52.00	0.00
18.50	0.00	0	52.00	0.00
19.00	0.00	0	52.00	0.00
19.50	0.00	0	52.00	0.00
20.00	0.00	0	52.00	0.00
20.50	0.00	0	52.00	0.00
21.00	0.00	0	52.00	0.00
21.50	0.00	0	52.00	0.00
22.00	0.00	0	52.00	0.00
22.50	0.00	0	52.00	0.00
23.00	0.00	0	52.00	0.00
23.50	0.00	Ö	52.00	0.00
24.00	0.00	0	52.00	0.00
0	3.00	J	2 0	

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Elevation Velocity

(ft/sec)

6.85

6.91

6.98

7.05

7.11

7.18

7.24

7.31

7.37

7.43

7.49

7.55

7.61

7.67

7.73

7.79

7.85

7.90

7.96

(feet)

54.60

54.65

54.70

54.75

54.80

54.85

54.90

54.95

55.00

55.05

55.10

55.15

55.20

55.25

55.30

55.35

55.40

55.45

55.50

Stage-Discharge for Reach 2R: Rip Rap Pool

Discharge

(cfs) 71.61

74.41

77.27

80.18 83.14

86.15

89.22

92.34

95.51

98.73

102.00

105.32

108.70 112.12

115.60

119.13

122.71

126.34

130.02

Clevation Clevet Clevet			,
52.00 0.00 0.00 52.05 0.60 0.02 52.10 0.95 0.08 52.15 1.24 0.18 52.20 1.50 0.34 52.25 1.73 0.54 52.30 1.94 0.80 52.35 2.14 1.10 52.40 2.32 1.47 52.45 2.50 1.88 52.50 2.67 2.36 52.55 2.83 2.88 52.60 2.98 3.46 52.65 3.13 4.10 52.70 3.28 4.79 52.75 3.41 5.53 52.80 3.55 6.33 52.85 3.68 7.19 52.90 3.80 8.10 52.95 3.93 9.07 53.00 4.04 10.09 53.05 4.16 11.17 53.15 4.39 13.49 53.20 4.49 <			
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4			3
54.45 6.64 63.51			1
54.50 6.71 66.16			
54.55 6.78 68.86	54.55	0.78	08.80

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Elevation End-Area

(feet)

54.60 54.65

54.70

54.75 54.80

54.85

54.90

54.95

55.00

55.05

55.10

55.15

55.20

55.25 55.30

55.35

55.40

55.45

55.50

Stage-Area-Storage for Reach 2R: Rip Rap Pool

(sq-ft) 10.5

10.8

11.1

11.4

11.7

12.0

12.3

12.6

13.0

13.3

13.6

13.9

14.3

14.6

15.0

15.3

15.6

16.0

16.3

Storage (cubic-feet)

105

108

111

114

117

120

123

126

130

133

136

139

143

146

150

153

156

160

163

Storage			•	
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53.45 4.4 44 53.50 4.6 46 53.55 4.8 48 53.60 5.0 50 53.65 5.3 53 53.70 5.5 55 53.75 5.8 58 53.80 6.0 60 53.85 6.3 63 53.90 6.5 65 53.95 6.8 68 54.00 7.1 71 54.05 7.3 73 54.10 7.6 76 54.15 7.9 79 54.20 8.1 81 54.25 8.4 84 54.30 8.7 87 54.40 9.3 93 54.45 9.6 96 54.50 9.9 99	53.35	3.9	39	
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POST DEVEL

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Printed 1/24/2022 Page 32

Summary for Pond 1P: 60 CONCRETE GALLEY'S

Inflow Area =	59,949 sf, 40.15% Impervious,	Inflow Depth >	4.09" for 25-YEAR event
Inflow =	3.23 cfs @ 12.49 hrs, Volume=	20,453 cf	
Outflow =	1.99 cfs @ 12.87 hrs, Volume=	17,871 cf,	Atten= 38%, Lag= 23.2 min
Discarded =	0.22 cfs @ 12.87 hrs, Volume=	12,033 cf	
Primary =	1.76 cfs @ 12.87 hrs, Volume=	5,838 cf	

Routing by Stor-Ind method, Time Span= 0.00-24.00 hrs, dt= 0.05 hrs Peak Elev= 62.39' @ 12.87 hrs Surf.Area= 2,269 sf Storage= 6,666 cf

Plug-Flow detention time= 157.9 min calculated for 17,834 cf (87% of inflow) Center-of-Mass det. time= 102.7 min (923.8 - 821.1)

Volume	Invert	Avail.Storage	Storage Description
#1A	58.33'	1,770 cf	18.60'W x 122.00'L x 5.17'H Field A
			11,724 cf Overall - 7,298 cf Embedded = 4,426 cf x 40.0% Voids
#2A	58.831	5,614 cf	Galley 4x8x4 x 60 Inside #1
			Inside= 42.0 "W x 43.0 "H => 12.47 sf x 7.50 'L = 93.6 cf
			Outside= 52.8 "W x 48.0 "H => 15.20 sf x 8.00 'L = 121.6 cf

7,384 cf Total Available Storage

Storage Group A created with Chamber Wizard

Device	Routing	Invert	Outlet Devices
#1	Primary	61.67'	12.0" Vert. Orifice/Grate C= 0.600
#2	Discarded	58.331	4.000 in/hr Exfiltration over Surface area
			Conductivity to Groundwater Elevation = 0.00'

Discarded OutFlow Max=0.22 cfs @ 12.87 hrs HW=62.39' (Free Discharge) —2=Exfiltration (Controls 0.22 cfs)

Primary OutFlow Max=1.75 cfs @ 12.87 hrs HW=62.39' (Free Discharge)

1=Orifice/Grate (Orifice Controls 1.75 cfs @ 2.89 fps)

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Page 33

Pond 1P: 60 CONCRETE GALLEY'S - Chamber Wizard Field A

Chamber Model = Galley 4x8x4

Inside= 42.0"W x 43.0"H => 12.47 sf x 7.50'L = 93.6 cf Outside= 52.8"W x 48.0"H => 15.20 sf x 8.00'L = 121.6 cf

52.8" Wide = 52.8" C-C Row Spacing

15 Chambers/Row x 8.00' Long = 120.00' Row Length +12.0'' End Stone x 2 = 122.00' Base Length 4 Rows x 52.8" Wide + 6.0" Side Stone x 2 = 18.60' Base Width 6.0" Base + 48.0'' Chamber Height + 8.0'' Cover = 5.17' Field Height

60 Chambers x 93.6 cf = 5,613.7 cf Chamber Storage 60 Chambers x 121.6 cf = 7,298.2 cf Displacement

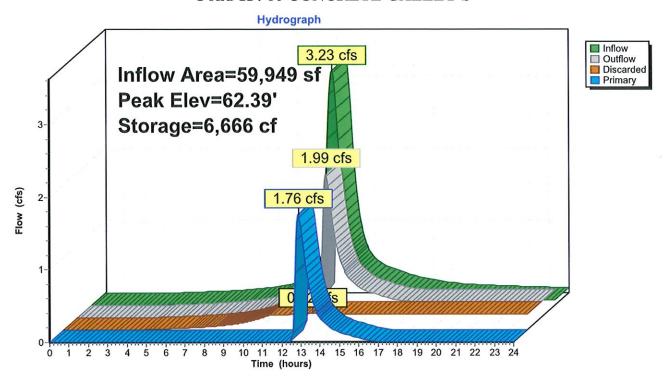
11,724.2 cf Field - 7,298.2 cf Chambers = 4,426.0 cf Stone x 40.0% Voids = 1,770.4 cf Stone Storage

Stone + Chamber Storage = 7,384.2 cf = 0.170 af Overall Storage Efficiency = 63.0%

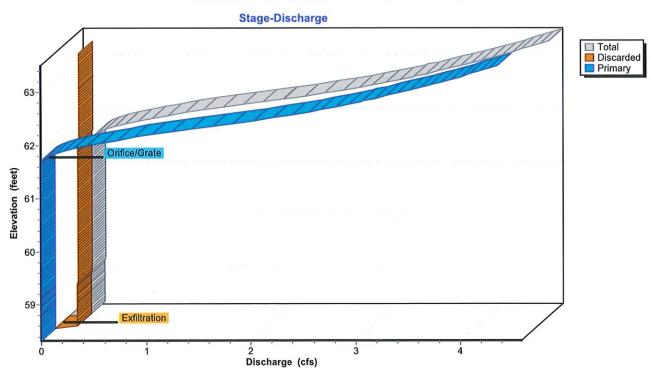
60 Chambers 434.2 cy Field 163.9 cy Stone



Pond 1P: 60 CONCRETE GALLEY'S



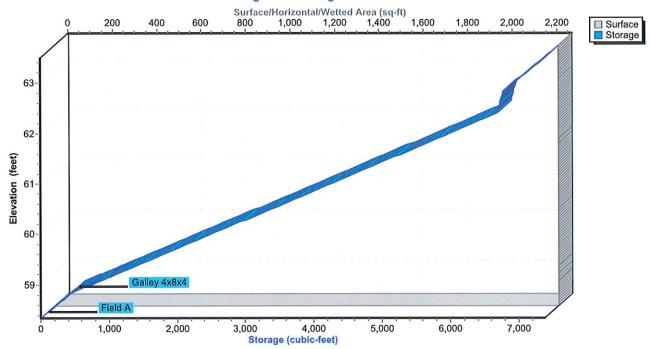
Pond 1P: 60 CONCRETE GALLEY'S



Printed 1/24/2022 Page 35

Pond 1P: 60 CONCRETE GALLEY'S

Stage-Area-Storage



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Hydrograph for Pond 1P: 60 CONCRETE GALLEY'S

Time	Inflow	Storage	Elevation	Outflow	Discarded	Primary
(hours)	(cfs)	(cubic-feet)	(feet)	(cfs)	(cfs)	(cfs)
0.00	0.00	0	58.33	0.00	0.00	0.00
0.50	0.00	0	58.33	0.00	0.00	0.00
1.00	0.00	0	58.33	0.00	0.00	0.00
1.50	0.00	0	58.33	0.00	0.00	0.00
2.00	0.00	0	58.33	0.00	0.00	0.00
2.50	0.00	0	58.33	0.00	0.00	0.00
3.00	0.00	0	58.33	0.00	0.00	0.00
3.50	0.00	0	58.33	0.00	0.00	0.00
4.00	0.01	1	58.33	0.00	0.00	0.00
4.50	0.01	2	58.33	0.01	0.01	0.00
5.00	0.01	3	58,33	0.01	0.01	0.00
5.50	0.02	4	58.33	0.02	0.02	0.00
6.00	0.02	5	58.34	0.02	0.02	0.00
6.50	0.03	6	58.34	0.03	0.03	0.00
7.00	0.04	8	58.34	0.04	0.04	0.00
7.50	0.05	10	58.34	0.05	0.05	0.00
8.00	0.06	13	58.34	0.06	0.06	0.00
8.50	0.07	16	58.35	0.07	0.07	0.00
9.00	0.09	20	58.35	0.09	0.09	0.00
9.50	0.12	25	58.36	0.11	0.11	0.00
10.00	0.15	33	58.37	0.15	0.15	0.00
10.50	0.19	42	58.38	0.19	0.19	0.00
11.00	0.26	78	58.42	0.21	0.21	0.00
11.50	0.36	247	58.60	0.21	0.21	0.00
12.00	0.92	834	59.05	0.21	0.21	0.00
12.50	3.23	4,427	61.10	0.22	0.22	0.00
13.00	1.54	6,588	62.35	1.81	0.22	1.59
13.50	0.70	6,125	62.08	0.88	0.22	0.66
14.00	0.48	5,909	61.95	0.56	0.22	0.34
14.50	0.38	5,798	61.89	0.43	0.22	0.21
15.00	0.33	5,725	61.85	0,36	0.22	0.14
15.50	0.28	5,667	61.81	0.32	0.22	0.09
16.00	0.24	5,608	61.78	0.28	0.22	0.06
16.50	0.20	5,537	61.74	0.24	0.22	0.02
17.00	0.18	5,457	61.69	0.23	0.22	0.00
17.50	0.16	5,361	61.64	0.22	0.22	0.00
18.00	0.14	5,233	61.56	0.22	0.22	0.00
18.50	0.12	5,073	61.47	0.22	0.22	0.00
19.00	0.12	4,891	61.37	0.22	0.22	0.00
19.50	0.11	4,697	61.26	0.22	0.22	0.00
20.00	0.10	4,493	61.14	0.22	0.22	0.00
20.50	0.10	4,281	61.02	0.22	0.22	0.00
21.00	0.09	4,060	60.89	0.22	0.22	0.00
21.50	0.09	3,833	60.76	0.22	0.22	0.00
22.00	0.09	3,599	60.63	0.22	0.22	0.00
22.50	0.08	3,358	60.49	0.22	0.22	0.00
23.00	80.0	3,110	60.35	0.22	0.22	0.00
23.50	0.07	2,856	60.20	0.22	0.22	0.00
24.00	0.07	2,595	60.05	0.22	0.22	0.00

Stage-Discharge for Pond 1P: 60 CONCRETE GALLEY'S

			_
Elevation	Discharge	Discarded	Primary
(feet)	(cfs)	(cfs)	(cſs)
58.33	0.00	0.00	0.00
58.43	0.21	0.21	0.00
58.53	0.21	0.21	0.00
58.63	0.21	0.21	0.00
58.73	0.21	0.21	0.00
58.83	0.21	0.21	0.00
58.93	0.21	0.21	0.00
59.03	0.21	0.21	0.00
59.13	0.21	0.21	0.00
59.23	0.21	0.21	0.00
59.33	0.21	0.21	0.00
59.43	0.21	0.21	0.00
59.53	0.21	0.21	0.00
59.63	0.21	0.21	0.00
59.73	0.22	0.22	0.00
59.83	0.22	0.22	0.00
59.93	0.22	0.22	0.00
60.03	0.22	0.22	0.00
60.13	0.22	0.22	0.00
60.23	0.22	0.22	0.00
60.33	0.22	0.22	0.00
60.43	0.22	0.22	0.00
60.53	0.22	0.22	0.00
60.63	0.22	0.22	0.00
60.73	0.22	0.22	0.00
60.83	0.22	0.22	0.00
60.93	0.22	0.22	0.00
61.03	0.22	0.22	0.00
61.13	0.22	0.22	0.00
61.23	0.22	0.22	0.00
61.33	0.22	0.22	0.00
61.43	0.22	0.22	0.00
61.53	0.22	0.22	0.00
61.63	0.22	0.22	0.00
61.73	0.24	0.22	0.02
61.83	0.33	0.22	0.11
61.93	0.50	0.22	0.28
62.03	0.74	0.22	0.52
62.13	1.04	0.22	0.81
62.23	1.38	0.22	1.15
62.33	1.75	0.22	1.52
62.43	2.13	0.22	1.90
62.53	2.49	0.23	2.27 2.58
62.63	2.81	0.23	
62.73	3.06	0.23	2.83
62.83	3.30	0.23	3.07 3.30
62.93	3,52	0.23	3.51
63.03 63.13	3.73 3.93	0.23 0.23	3.71
63.13	4.12	0.23	3.89
63.23	4.12	0.23	3.89 4.07
63.43	4.47	0.23	4.24
03,43	7.7/	U.23	च∙‰चे

Stage-Area-Storage for Pond 1P: 60 CONCRETE GALLEY'S

Elevation	Surface	Storage
(feet)	(sq-ft)	(cubic-feet)
58.33	2,269	0
58.43	2,269	91
58.53	2,269	182
58.63	2,269	272
58.73	2,269	363
58.83	2,269	454
58.93	2,269	624
59.03	2,269	794
59.13	2,269	969
59.23	2,269	1,146
59.33	2,269	1,322
59.43	2,269	1,499
59.53	2,269	1,675
59.63	2,269	1,852
59.73	2,269	2,028
59.83	2,269	2,204
59.93	2,269	2,380
60.03	2,269	2,555
60.13	2,269	2,731
60.23	2,269	2,906
60.33	2,269	3,082
60.43	2,269	3,257
60.53	2,269	3,432
60.63	2,269	3,607
60.73	2,269	3,781
60.83	2,269	3,956
60.93	2,269	4,130
61.03	2,269	4,305
61.13	2,269	4,479
61.23	2,269	4,653
61.33	2,269	4,827
61.43	2,269	5,000
61.53	2,269	5,174
61.63	2,269	5,347
61.73	2,269	5,521
61.83	2,269	5,694
61.93		
62.03	2,269	5,867
	2,269	6,040
62.13	2,269	6,212
62.23	2,269	6,385
62.33	2,269	6,558
62.43	2,269	6,699
62.53	2,269	6,719
62.63	2,269	6,739
62.73	2,269	6,759
62.83	2,269	6,779
62.93	2,269	6,870
63.03	2,269	6,961
63.13	2,269	7,051
63.23	2,269	7,142
63.33	2,269	7,233
63.43	2,269	7,324

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Page 39

Summary for Link 1L: POC "A" DRAIN INLET AT S.E. END OF PARCEL

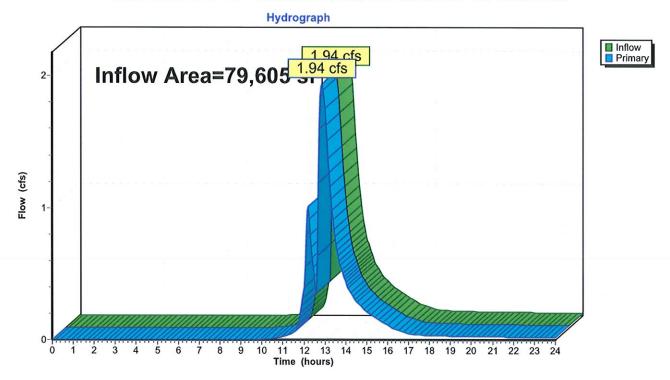
Inflow Area = 79,605 sf, 30.24% Impervious, Inflow Depth > 1.49" for 25-YEAR event

Inflow = 1.94 cfs @ 12.88 hrs, Volume= 9,858 cf

Primary = 1.94 cfs @ 12.88 hrs, Volume= 9,858 cf, Atten= 0%, Lag= 0.0 min

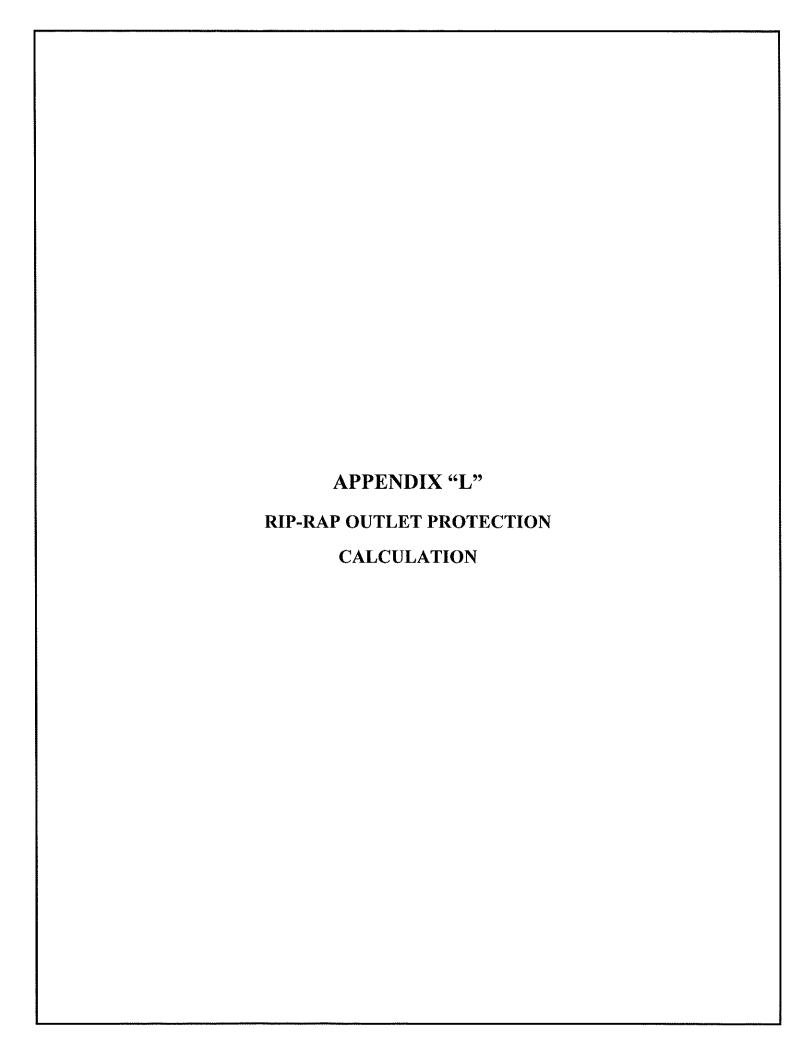
Primary outflow = Inflow, Time Span= 0.00-24.00 hrs, dt= 0.05 hrs

Link 1L: POC "A" DRAIN INLET AT S.E. END OF PARCEL



Hydrograph for Link 1L: POC "A" DRAIN INLET AT S.E. END OF PARCEL

			_				
Time	Inflow	Elevation	Primary	Time	Inflow	Elevation	Primary
(hours)	(cfs)	(feet)	(cfs)	(hours)	(cfs)	(feet)	(cfs)
0.00	0.00	0.00	0.00	13.00	1.76	0.00	1.76
0.25	0.00	0.00	0.00	13.25	1.16	0.00	1.16
0.50	0.00	0.00	0.00	13.50	0.78	0.00	0.78
0.75	0.00	0.00	0.00	13.75	0.56	0.00	0.56
1.00	0.00	0.00	0.00	14.00	0.44	0.00	0.44
1.25	0.00	0.00	0.00	14.25	0.35	0.00	0.35
1.50	0.00	0.00	0.00	14.50	0.29	0.00	0.29
1.75	0.00	0.00	0.00	14.75	0.25	0.00	0.25
2.00	0.00	0,00	0.00	15.00	0.21	0.00	0.21
2.25	0.00	0.00	0.00	15.25	0.19	0.00	0.19
2.50	0.00	0.00	0.00	15.50	0.16	0.00	0.16
2.75	0.00	0.00	0.00	15.75	0.13	0.00	0.13
3.00	0.00	0.00	0.00	16.00	0.11	0.00	0.11
3.25	0.00	0.00	0.00	16.25	0.09	0.00	0.09
3.50	0.00	0.00	0.00	16.50	0.07	0.00	0.07
3.75	0.00	0.00	0.00	16.75	0.06	0.00	0.06
4.00	0.00	0.00	0.00	17.00	0.05	0.00	0.05
4.25	0.00	0.00	0.00	17.25	0.04	0.00	0.04
4.50	0.00	0.00	0.00	17.50	0.04	0.00	0.04
4.75	0.00	0.00	0.00	17.75	0.04	0.00	0.04
5.00	0.00	0.00	0.00	18.00	0.03	0.00	0.03
5.25	0.00	0.00	0.00	18.25	0.03	0.00	0.03
5.50	0.00	0.00	0.00	18.50	0.03	0.00	0.03
5.75	0.00	0.00	0.00	18.75	0.03	0.00	0.03
6.00	0.00	0.00	0.00	19.00	0.03	0.00	0.03
6.25	0.00	0.00	0.00	19.25	0.03	0.00	0.03
6.50	0.00	0.00	0.00	19.50	0.03	0.00	0.03
6.75	0.00	0.00	0.00	19.75	0.03	0.00	0.03
7.00	0.00	0.00	0.00	20.00	0.03	0.00	0.03
7.25	0.00	0.00	0.00	20.25	0.03	0.00	0.03
7.50	0.00	0.00	0.00	20.50	0.03	0.00	0.03
7.75	0.00	0.00	0.00	20.75	0.03	0.00	0.03
8.00	0.00	0.00	0.00	21.00	0.02	0.00	0.02
8.25	0.00	0.00	0.00	21.25	0.02	0.00	0.02
8.50	0.00	0.00	0.00	21.50	0.02	0.00	0.02
8.75	0.00	0.00	0.00	21.75	0.02	0.00	0.02
9.00	0.00	0.00	0.00	22.00	0.02	0.00	0.02
9.25	0.00	0.00	0.00	22.25	0.02	0.00	0.02
9.50	0.00	0.00	0.00	22.50	0.02	0.00	0.02
9.75	0.00	0.00	0.00	22.75	0.02	0.00	0.02
10.00	0.00	0.00	0.00	23.00	0.02	0.00	0.02
10.25	0.01	0.00	0.01	23.25	0.02	0.00	0.02
10.50	0.01	0.00	0.01	23.50	0.02	0.00	0.02
10.75	0.02	0.00	0.02	23.75	0.02	0.00	0.02
11.00	0.02	0.00	0.02	24.00	0.02	0.00	0.02
11.25	0.04	0.00	0.04				
11.50	0.06		0.06	1			
11.75	0.13	0.00	0.13				
12.00	0.40		0.40				
12.25	0.92		0.92				
12.50	0.48		0.48				
12.75	1.60	0.00	1.60	I			



Fuller Engineering & Land Surveying

525 John Street • Second Floor Bridgeport, CT 06604 (203) 333-9465 (203) 336-1769 FAX

Project: 245 NORWICH NEW LONDON ROAD

MONTVILLE, CT

Date: 1/24/22

Rip - Rap Outlet Protection Calculation

Complete

d By: SDU

Drainage Checked

Area: (1P) 60 4x8 CONCRETE GALLEYS By:

Ref. Section 7.3 CONNDOT Drainage Manual.

La = Length of Apron (Type A Riprap Apron - Minimum Tailwater Condition TW < 0.5 Rp

$$L_a = \frac{1.80 (Q - 5)}{Sp^{1.5}}$$

where:

La = length of apron, m (ft)

 S_p = inside diameter for circular sections or maximum inside pipe span for noncircular sections, (ft)

Q = pipe (design) discharge, (cfs) = 1.94 cfs = 12'' (1.0 ft)

TW = tailwater depth, (ft) = 0 (free discharge)

 R_p = maximum inside pipe rise, (ft) = 1.0'

Note: $S_p = R_p$ = inside diameter for circular sections

Type A Riprap Apron (Minimum Tailwater Condition) L_a = 1.03 ft

 $W_1 = 3S_p \text{ (min.)}$ 3 ft

 $W_2 = 3s_p + 0.7L_a$ for TW < 0.5 R_p 3.72 ft

where:

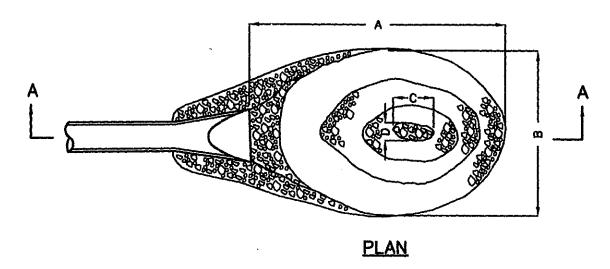
 W_1 = width of apron at pipe outlet or upstream apron limit W_2 = width of apron at terminus or downstream apron limit

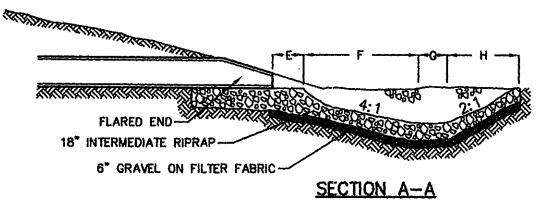
Therefore a Type A Riprap apron with dimensions as follows is required:

3 ft W + 4 ft W x 4 ft L

Provided is a Pre-formed Scour Hole with dimensions as follows:

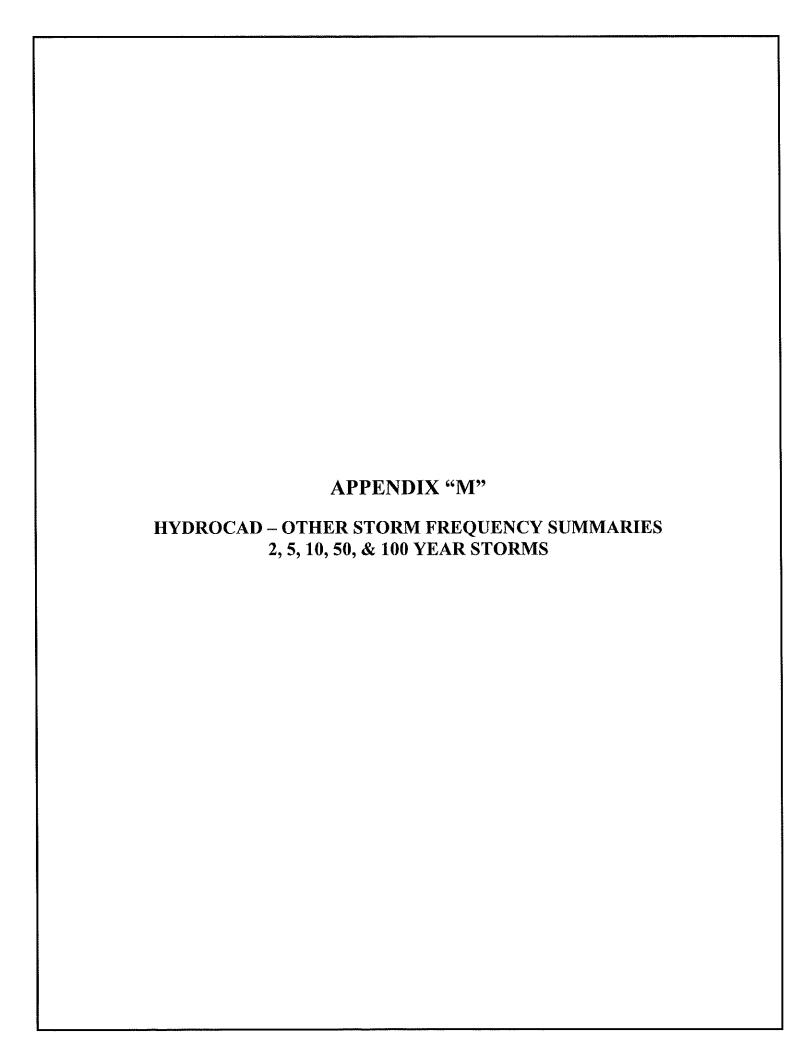
7.0 ft W x 10.0 ft L x 1.5 ft D > the required apron therefore <u>OK</u>



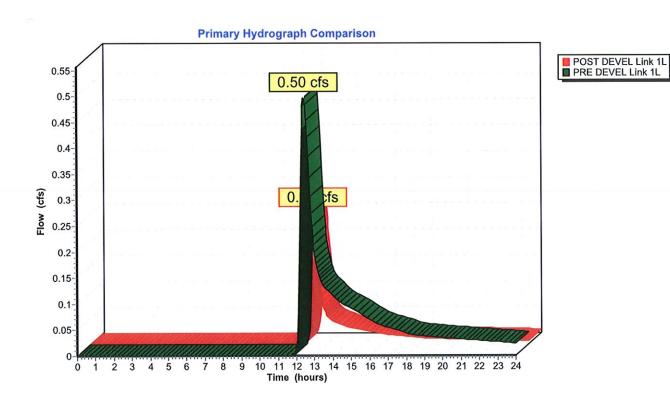


RIPRAP PLUNGE POOL

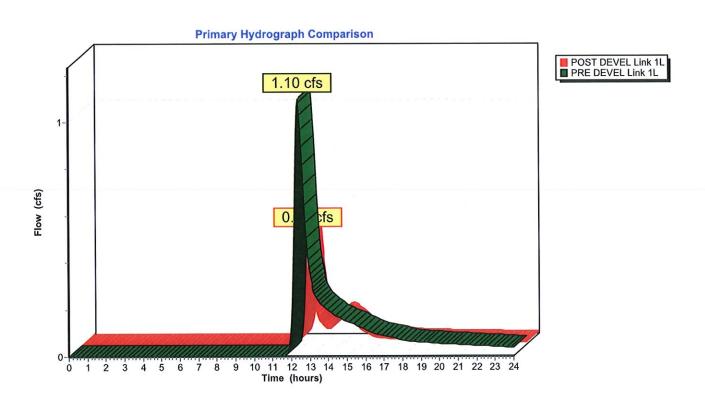
PIPE SIZE	Α	В	С	D	E	F	G	Н	WT. RIPRAP TONS
12"&15"	10'	7'	1'-6"	1'	1'	4'-6"	1'-6"	3'	6
18"	12'	8'	2'	1'	1'	5'	2'	4'	8
21"	15'	9'	2'-6"	1'-6"	1'	7'	2'-6"	4'-6"	12
24"	17'	10'	2'-6"	1'-6"	1'	8'	2'-6"	5'~6"	15
30"	20'	13'	3'	2'	2'	9'	3'	6'	22
36"	24'	16'	3'-6"	2'	2'	9'-6"	3'-6"	7'	33



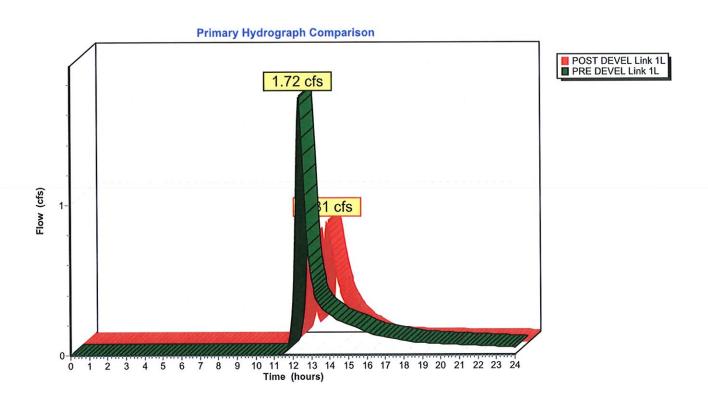
Node	Inflow	Primary
	(cfs)	(cfs)
POST DEVEL Link 1L	0.25	0.25
PRE DEVEL Link 1L	0.50	0.50



Node	Inflow	Primary
	(cfs)	(cfs)
POST DEVEL Link 1L	0.48	0.48
PRE DEVEL Link 1L	1.10	1.10

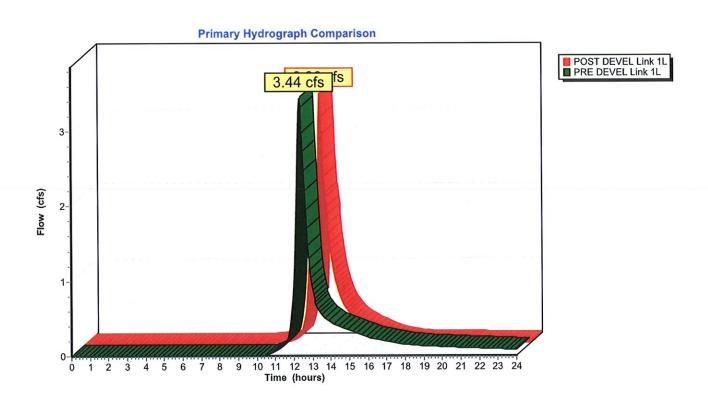


Node	Inflow	Primary
	(cfs)	(cfs)
POST DEVEL Link 1L	0.81	0.81
PRE DEVEL Link 1L	1.72	1.72

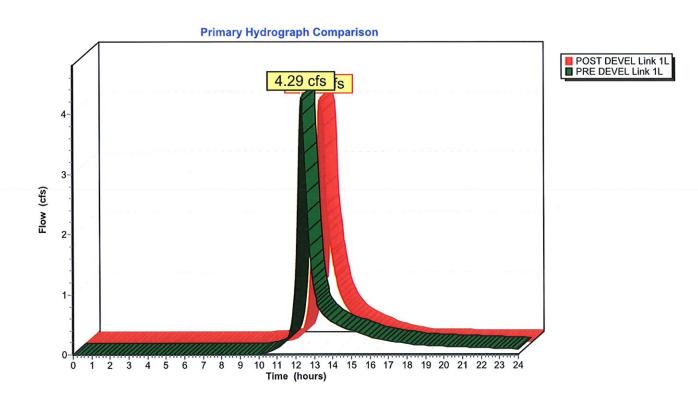


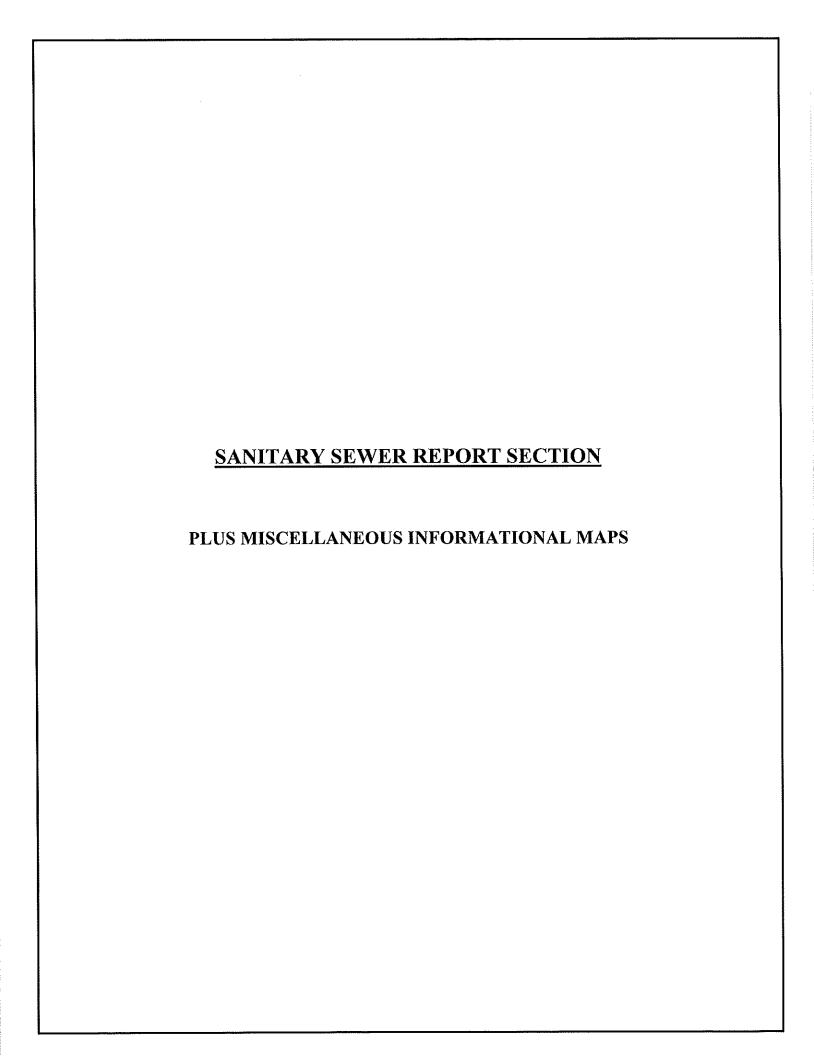
Prepared by Fuller Engineering & Land Surveying, LLC HydroCAD® 10.00 s/n 02123 © 2011 HydroCAD Software Solutions LLC

Node	Inflow	Primary
	(cfs)	(cfs)
POST DEVEL Link 1L	3.36	3.36
PRE DEVEL Link 1L	3.44	3.44



Node	Inflow	Primary
	(cfs)	(cfs)
POST DEVEL Link 1L	4.07	4.07
PRE DEVEL Link 1L	4.29	4.29





FULLER ENGINEERING AND LAND SURVEYING, LLC 525 John Street – Second Floor – Bridgeport, CT 06604

Phone: (203) 333-9465 Fax: (203) 336-1769

PROJECT: RESIDENTIAL DEVELOPMENT @ #245 ROUTE 32 LOCATION: 245 NORWICH-NEW LONDON ROAD (ROUTE 32)

CLIENT: WESTERN GROUP, LLC

SUMMATION OF PROPOSED SEWAGE FLOW:

	QTY (unit or sqft)	GPD/UNIT	TOTAL GPD	
STUDIO	0	200	-	
1 BEDROOM	0	200	-	
2 BEDROOM	0	300	-	
3 BEDROOM	22	400	8,800.00	
			-	
TOTAL	22		8,800.00	GPD
	7.48 GAL	1 CF	1,176.47	CF/day
	1 day	24 hour	49.01960784	CF/HR
	1 hour	3600 sec	0.013616558	CFS
	MGD=	0.00880	MGD*4=	0.0352
INCLUDE PEAKING F	ACTOR OF 4		0.054466231	CFS

where:

GPD = Gallons per Day

MGD = Millions Gallons per Day

<u>Note:</u> The Existing house is to remain unchanged with 3 Bedrooms in addition to 21 residential apartment units each with 3 bedrooms.

FULLER ENGINEERING AND LAND SURVEYING, LLC 525 John Street – Second Floor – Bridgeport, CT 06604

Phone: (203) 333-9465 Fax: (203) 336-1769

CONVEYANCE CALCULATIONS:

PROJECT: RESIDENTIAL DEVELOPMENT @ #245 ROUTE 32

LOCATION: 245 NORWICH-NEW LONDON ROAD (ROUTE 32) MONTVILLE, CT

CLIENT: WESTERN GROUP, LLC

PIPE: Existing 8" Sanitary Sewer in Town Road

Pipe Diameter: 8 inches

MANNINGS EQUATION

R = ___A ___ 0.166667

Pw

Where R: Hydraulic radius (ft)

A: Cross-sectional area (ft 2) 0.349066 P_W : Wetted Perimeter (ft) 2.094395

 $V = \frac{k R^{2/3} S^{1/2}}{n} 2.452942$

Where V: Mean Velocity (ft/s) k: 1.49 for U.S. customary units, or 1.0 for S.I. units

n: Manning's roughness value 0.012
R: Hydraulic Radius (ft) 0.166667

S: friction Slope (ft/ft) 0.004255

Q= VA 0.856238 cfs

Where Q: Flow Rate(cfs)

V: Average velocity (ft/s)

The Q for the proposed buildings plus storm infiltration going in to the system is 0.054 cfs which is less than the calculated Q; therefore OK The Existing 8" Lateral at 0.0043 slope is adequate.

Notes:

- 1. Storm runoff infiltration is considered at part of the safety factor.
- 2. Sewer system from development will be a force main system. Each building complex is to have a separate Grinder Pump System as Mfg. by e-ONE Sewer Systems.



Table 1 - Average Daily Flow on Specific Developments

TYPE OF DEVELOPMENT	UNIT	ADF (GPD/UNIT)
Auditorium	Seat	5
Automobile parking	1000 Gross square feet	25
Automobile repair garage	1000 Gross square feet	100
Bar	Seat	20
Bar: Public Areas & Tables	15 Gross square feet	20
Barber Shop	1000 Gross square feet	50
Beauty Salon	1000 Gross square feet	200
Carwash	Square feet inside	240
Church	Seat	5
Community center	Occupant	5
Country Club	Member	20
Factories (Exclusive of industrial waste)	Employee/shift	25
Factories (add for showers)	Employee/shift	+10
Gymnasium	1000 Gross square feet	300
Hospital - Convalescent/Rest Homes	Bed	150
Hospital	Bed	250
Jail	Inmate	85
Laboratory - commercial	1000 Gross square feet	300
Laundromat	Washer	400
Library / Museum	1000 Gross square feet	25
Manufacturing - industry	1000 Gross square feet	100
Medical building	1000 Gross square feet	300
Motel/Hotel	Room	100
Motel/Hotel (with cooking facilities)	Room	150
Office building	1000 Gross square feet	200
Residential -	Dwelling unit	400
- single family dwelling, Townhouses	Dwelling unit Dwelling unit	100
bachelor/single, artist dwelling1 Bedroom apartment or condo	Dwelling unit	200
- 2 Bedroom apartment or condo	Dwelling unit	300
- 3 Bedroom apartment of condo	Dwelling unit	400
- boarding house	Bed	85
- mobile home	Unit	200
- guest house with kitchen	Dwelling unit	300
Restaurant - fixed seat	Seat	50 or
Restaurant (dining area)	15 Gross square feet	50
Restaurant - Bakery, Doughnut Shop, take out	1000 Gross square feet	300
School - day care center	Child	10
School - elementary / junior high	Student	10
School - high school	Student	15
School - kindergarten	35 Gross square feet	10
Stadium/Theater - fixed seat	Seat	5
Stores, Shopping Centers, and Malls	1000 Gross square feet	100
University or College	Student	20
University Dormitory	Student	100
Veterinarian	1000 Gross square feet	300
Warehouse	1000 Gross square feet	25



Table 1 Notes:

Gross square feet: area included within the exterior of the surrounding walls of a building excluding courts.

Example Calculation - Assume a 10,000 sq. ft. office building is proposed. The estimated average daily flow is calculated as 10,000 sq. ft. x 200 gpd/1000 sq. ft. = 2000 gpd.

Table 2 - Average Flow Rate based on Land Use and Area Density

LAND USE / AREA DENSITY	UNIT	ADF (GPD/UNIT)
Low Density Residential (Single Family) (10 people / acre)	acre	1,000
Medium Density (Multi-Family) Residential (12 to 15 people / acre)	acre	1,200 - 1,500
High Density (Multi-Family) Residential (20 to 75 people / acre)	acre	2,000 - 7,500
Office & Institutional	acre	5,000
Commercial & Light Industrial	acre	5,000
Industrial	acre	10,000

The design Flow shall be calculated as follows:

Design Flow = Average Daily Flow x Peaking Factor

where:

Design Flow = Flow used to design a sanitary sewer facility, gpd.

Average Daily Flow = Estimated average daily flow, gpd.

Peaking Factor = Ratio of peak hourly flow to average daily flow. A peaking factor of four (4) shall be used for all calculations unless directed otherwise by the Authority.

Note:

All developments with proposed ADF above 2,000 gpd are required to evaluate the capacity of the existing sanitary sewer system.

PVC SEWER & STORM DRAINAGE PIPE

Scope: This submittal designates the general requirements for Unplasticized Polyvinyl Chloride (PVC) Plastic

PSM Sewer Pipe from compound with a cell classification 12454, as defined in ASTM Standard D-

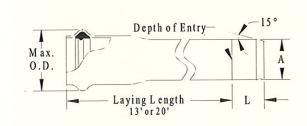
1784.

Pipe: Pipe in trade size diameter of 4" through 15" shall meet the requirements of the latest ASTM D-3034

Standard. Pipe in trade sizes diameter of 18" and above shall meet the requirements of the latest ASTM Standard F-679. The above pipe shall conform to the requirements of CSA B-182.2. If integral gasketed bell ends are provided on the pipe, the pipe joint must meet the requirements of ASTM Standard D-3212, and the sealing gasket must conform to the requirements of ASTM Standard F-477 for sizes 4"-15". The D-3034 normal pipe length will be 13'+/-1" laying length, (BNQ: 13'1½" min.) with other lengths

available upon request. Pipe in trade size diameters of 4 and 6 inch are available with solvent-weld bells.

Fittings: Fittings shall conform to ASTM D-3034 & F-679 & CSA B-182.2.



Pipe Dimensions

AS	TM D-30	34			nimum Wall	SIGNED CONTROL OF		"L" Dimension Reference
Nominal Size	Metric (m.m)	Average O.D.	SDR-41	SDR-35	SDR-26	SDR-23.5	Max. Bell OD	Max.
4"	100	4.215		0.120	0.162	0.178	5.050	3.500
6"	150	6.275	0.153	0.180	0.241	0.265	7.305	4.375
8"	200	8.400	0.205	0.240	0.323		9.605	4.375
10"	250	10.500	0.256	0.300	0.404		12.030	6.125
12"	300	12.500	0.305	0.360	0.481		14.100	6.000
15"	375	15.300	0.375	0.437	0.588		17.200	6.375
Min. Pipe			28 psi	46 psi	115 psi	153 psi		
A	STM F-67	79	200	Min. R-35)	*T-1 Min. (SDR-26)	**T-2 Min (SDR-35)		
18"	450	18.701	0.	536	0.719	0.499	20.690	9.125
21"	500	22.047	0.	632	0.847	0.588	24.260	10.125
24"	600	24.803	0.	711	0.953	0.661	27.290	11.125
Min. Pipe @ 5% Def		•	46	psi	115 psi	46 psi		

^{*}T-1 Is for material with a minimum cell classification of 12454B (400,000 psi min. modulus).
**T-2 Is for material with a minimum cell classification of 12364C (500,000 psi min. modulus).
This information is for reference only and is not manufactured by National Pipe & Plastics, Inc.

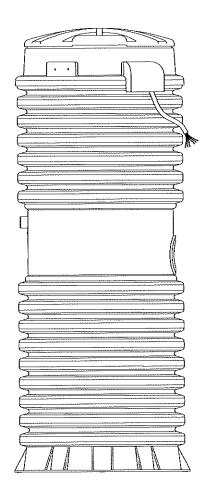












Low Pressure
Sewer Systems
Using
Environment One
Grinder Pumps

Contents

3
3
3
4
4
5
7
7
9
9
9
10
10
11
12
14
17
22
30

Introduction

E/One low pressure sewer (LPS) systems offer the designer new freedom in solving many problem situations that have defied reasonably economical solutions using the conventional approach.

Each LPS system design should be considered on the basis of its own unique circumstances. On such a basis, a sound choice between gravity and low pressure systems can be made.

General criteria aid the engineer in making a preliminary choice between several alternative systems: entirely low pressure, entirely gravity, entirely vacuum or a combination of systems. These criteria are presented and are intended to serve as a general guide. The final decision and design are the responsibility of the project consulting engineer, whose knowledge of local conditions, including construction costs, regulatory requirements and the client's particular needs, become vital to the preparation of the final designs and specifications.

Advantages of LPS Systems

LPS systems have low initial (front end) cost compared to gravity systems, which have nearly all the total investment allocated in the first stage. With the LPS system, grinder pump costs are incurred only as construction progresses. These costs will be deferred for many years in certain types of development programs.

An LPS system is not subject to infiltration from ground water or from surface storm water entering through leaking pipe joints and manholes. With zero infiltration, treatment plants need not be sized to handle the peak flow rates caused by infiltration. Treatment efficiencies can be more consistent, and treatment plant operating costs decrease.

An LPS system may become the critical factor in determining whether "marginal" land can be economically developed. Many attractive sites have been considered unsuitable for development because of the excessive costs typically associated with conventional sewer systems — sites with hilly terrain, land with negligible slope, high water tables, poor percolation characteristics, rock, seasonal occupancy or low population density.

Many communities are planning to convert from septic tanks to central sewage collection and treatment systems to minimize health hazards and/or environmental deterioration. The major reduction in cost and the simplicity of installation of an LPS system have strong appeal for such community improvement programs. Small-diameter pipe pressure mains can be laid along existing roadways with minimum disruption to streets, sidewalks, lawns, driveways and underground utilities. Surface restoration costs are similarly minimized. Sewage delivered to the treatment plant (because it contains no infiltration) is more uniform in "strength," the volume is smaller, and peaks are greatly reduced.

Description and Operation

Grinder pumps of approved design accomplish all pumping and sewage-grinding processes for small-diameter LPS systems.

The system consists of conventional drain, waste and vent (DWV) piping within the residence connected to the grinder pump inlet. The grinder pump may be installed above or below grade, indoors or outdoors. Depending on flow factors and model used, it may serve one or more resi-

dences, or several families in the case of apartment buildings.

Grinder pumps discharge a finely ground slurry into small-diameter pressure piping. In a completely pressurized collection system, all the piping downstream from the grinder pump (including laterals and mains) will normally be under low pressure. Pipe sizes will start at 1 1/4 inches for house connections (compared to 4 or 6 inches in gravity systems) and will be proportionally smaller than the equivalent gravity pipeline throughout the system. All pipes are arranged as zone networks without loops.

Depending on topography, size of the system and planned rate of buildout, appurtenances may include valve boxes, flushing arrangements, air release valves at significant high points, check valves and full-ported stops at the junction of each house connection with the low pressure sewer main.

Pump Operation

Low pressure sewer systems have become feasible with the availability of the Environment One grinder pump, the reliability of which has been proven in almost 40 years of service. The grinder pump station provides adequate holding capacity, reliable grinding and pressure transport of a fine slurry to an existing gravity sewer, pump station or directly to a wastewater treatment plant.

In operation, the grinder pump station will handle sewage and many items that should not, but often do, appear in domestic wastewater. For example, plastic, wood, rubber and light metal objects can be routinely handled without jamming the grinder or clogging the pump or piping system. The grinder pump will discharge this slurry at a maximum rate of 15 gpm or 11 gpm at a pressure of 40 psig. Transporting sewage several thousand feet to a discharge point at a higher elevation is possible as long as the sum of the static and friction losses does not exceed design limits of 185 feet TDH (80 psig).

The grinder pump is actuated when the depth of the sewage in the tank reaches a predetermined "turn-on" level, and pumping continues until the "turn off" level is reached. The pump's running time is short, power consumption is low, and long pump life is ensured. The unit is protected against backflow from discharge lines by an integral check valve. Several grinder pump station models are available to satisfy various total and peak demand conditions.

Pump Type

The semi-positive displacement pump in the grinder pump station has a nearly vertical H-Q curve. This is the best type of pump for successful parallel operation of many pumps into a system of common low pressure mains. Since each pump will be located at a different point along common low pressure mains and at various elevations, each pump should operate in an efficient and predictable manner, whether one pump or numerous pumps are operating at a given moment; the pumps in such a system do not have a single fixed "operating point," but must operate consistently over a wide range of heads that are continually, and often rapidly, changing.

The Environment One grinder pump has the capability of operating above the LPS system design criteria of 80 psig, or 185 feet (Figure 1). Based on the maximum daily number of pumps operating simultaneously (Table 3) versus the number of pumps connected to the system at the design pressure of 185 feet, the capability to operate significantly above the system's design pressure is mandatory in order for the system to operate properly during the approximately bimonthly peaks when

the "absolute maximum" numbers of pumps are operating. This feature also ensures that pumping will continue under those conditions when higher–than–normal pressure occurs in the pipeline.

System designs with calculated heads approaching the upper limits of recommended heads should be reviewed by Environment One application specialists. Contact your local Environment One Regional Sales Office or authorized distributor for a no-cost, computerized review of your design.

Occasionally during "normal" operation, there will be short periods when higher-than-design pressures will be experienced. These can result from a variety of causes including solids buildup (obstructions) or air bubbles.

Deposits of solids or air accumulation will be purged from the line since the pump continues to produce an essentially constant flow, even though the cross section of the pipeline has temporarily been reduced. Higher velocities through the reduced cross section will provide the scouring action needed to correct such conditions as soon as they start to appear.

These higher—than—expected pressure conditions are transitory occurrences. The only requirement is that no damage be done to the pumping equipment, pipelines or appurtenances during these occasional short periods. Environment One grinder pumps are driven by motors rated for continuous operation at 104 F/40 C above ambient temperature. They can operate at 50 percent above rated pressure for at least 5 minutes without excessive temperature rise. Based on the Albany, New York, demonstration project⁴, for this type of overload to last even as long as one minute would be rare.

Motor Selection

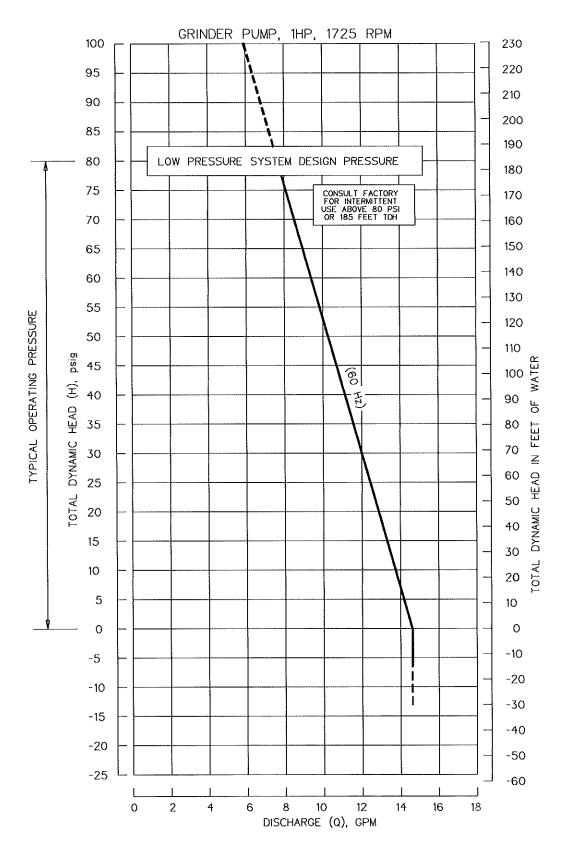
A grinder pump station is an electromechanical system that depends on electric power for its operating, control and alarm functions. The design and selection of Environment One's pump, motor, grinder and level—sensing controls were accomplished by optimizing the wastewater transport function of the unit within the necessary constraints for unattended, trouble—free operation in a residential environment.

A single grinder pump core is common to all models of Environment One grinder pumps (models DH071, DH151, DH152, DH272 and DH502). This central core contains all of the working and control elements of the unit and is powered by a 1 hp, 240v (or 120v), 1,725 rpm capacitor start, thermally protected induction motor. Each of these motor features was carefully considered in the design of the grinder pump station.

The pump should be considered as a residential appliance. For this reason, performing the grinding and pumping functions using no more than 1 hp to permit occasional use at 120v in older homes not wired for 240v is desirable. In order to achieve the high heads desired and provide constant flow at varying heads, the 1-hp motor is coupled to a pump of semi-positive displacement design (Figure 1).

At a rating of 1 hp and 1,725 rpm, the Environment One grinder pump develops more than 8.4 foot-pounds of torque. Motors used to drive centrifugal pumps are often rated at 2.0 hp at 3,450 rpm and may produce less torque. When handling residential sewage, grinding torque may be demanded during any portion of the starting or running cycle. When the pump stops (controlled by level) in the midst of grinding hard objects (e.g. tongue depressors, plastic items, etc.), it must, upon restarting, be able to provide sufficient torque to the grinder to overcome the resistance of any object remaining from the previous cycle.

Grinder Pump Performance Characteristics



Power Outages

Environment One grinder pump stations have adequate excess holding capacity to provide wastewater storage during most electrical power outages (Figure 2). This excess holding capacity is shown on curve A. Data from the Federal Power Commission on national electrical power outages is plotted as a cumulative distribution function (curve B). Note that only volume above the normal "turn-on" level was counted as available storage. The average flow of 1.54 gallons/hour/person is based on the actual measured flow over a one-year period at the Albany Demonstration Project⁴.

The local electrical power utility should be contacted to obtain a history on the power interruptions of the feeder(s) scheduled to serve the low pressure sewer site. From this data, curve B should be replotted to reflect local conditions. In those rare local areas where the frequency and/or the duration of outages exceed 7.5 hours, the use of Model DH151, with its greater holding capacity than that of the DH071, could be considered.

When power has been restored after a power outage, it is likely that nearly all the pumps in the system will try to operate simultaneously. Under these conditions, the dynamic head loss component of the total head will rise significantly. A number of pumps in the system would see a total back pressure high enough to cause the thermal overload protectors to automatically trip in a few minutes. Operation under conditions that could cause damage to the pumps or the system would be avoided. While these pumps are offline, other pumps in the system would be able to empty their tanks. After one to two minutes, the group that tripped off on thermal overload would cool and restart. The system back pressure would have been reduced and the group would be able to pump down normally. This process repeats itself automatically under the influence of each unit's own thermal protector, reliably restoring the system to normal operation.

Power Consumption

Monthly power consumption of a residential grinder pump station is substantially less than that of other major appliances. The power consumption will vary based on the system operating parameters. The monthly cost can be approximated using the following equation and operating data:

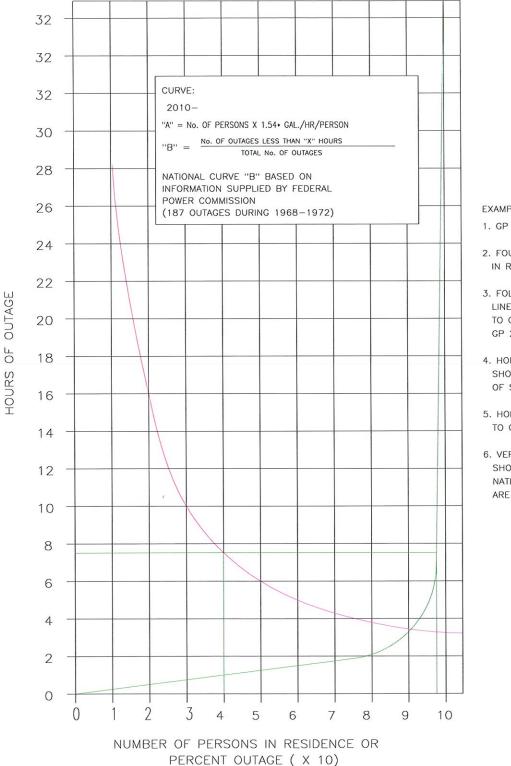
Discharge Pressure (PSI)	0	25	60	80
* Watts	690	770	1100	1400
** Flow (GPM)	15	12.4	9.3	7.7

As an example of the calculation for a typical single-family home using 250 GPD, pumping at 25 psi is:

Then, multiply the kilowatt hours by the current cost of electricity and you will have an approximate monthly cost of running the unit.

Figure 2

Relationship of GP Storage Capacity to Power Outage Experience



EXAMPLE:

- 1. GP 2010 INSTALLED
- 2. FOUR PERSONS IN RESIDENCE
- 3. FOLLOW VERTICAL LINE 4 UPWARD TO CURVE "A" FOR GP 2010
- 4. HORIZONTALLY LEFT SHOWS 7-1/2 HOURS OF STORAGE CAPACITY
- 5. HORIZONTALLY RIGHT TO CURVE "B"
- 6. VERTICALLY DOWN SHOWS 97% OF THE NATIONS OUTAGES ARE SATISFIED

LPS System Design

Once the initial analysis of a project has confirmed the feasibility of using the low-pressure approach, the completion of a preliminary system design is straightforward. This is primarily a result of two characteristics of E/One's semi-positive displacement pump: near-constant flow over the entire range of operating pressures and the ability of the pump to handle transient overpressures.

The balance of this section outlines a systematic approach to LPS system design, leading from pump model and pipe selection to a detailed zone and system analysis.

Information Required

The information that should be assembled prior to initiation of the LPS system design includes:

- Topography map
- Soil conditions
- Climatic conditions (frost depth, low temperature and duration)
- Water table
- Applicable codes
- Discharge location
- Lot layout (with structures shown, if available)
- · Total number of lots
- Dwelling type(s)
- Use and flow factors (seasonal occupancy or year-round, appliances, water supply sources)
- Area development sequence and timetable

Grinder Pump Station Size Selection

Use this table to select grinder pump models for the types of occupancy to be served.

Model	Recommended Flow (gpd)	Adequate for Managing
DH071	up to 700	Flow from one average single-family home, and up to two average, single-family homes where codes allow and with consent of the factory.
DH151	up to 1,500	Flow from up to two average single-family homes, and up to six average, single-family homes where codes allow and with consent of the factory.
DH152	up to 3,000	Flow from up to four average single-family homes, and up to 12 average, single-family homes with consent of the factory.
DH272	up to 5,000	Flow from up to six average single-family homes, and up to 20 average, single-family homes with consent of the factory.
DH502	up to 6,000	Flow from up to nine average single-family homes,

and up to 24 average, single-family homes with consent of the factory.

Considerations include:

- Wetwell and discharge piping must be protected from freezing
- · Model and basin size must be appropriate for incoming flows, including peak flows
- · Appropriate alarm device must be used
- Suitable location

Daily flows above those recommended may exceed the tank's peak flow holding capacity and/or shorten the interval between pump overhauls. The company should be consulted if higher inflows are expected.

The final selection will have to be determined by the engineer on the basis of actual measurements or best estimates of the expected sewage flow.

Grinder Pump Placement

The most economical location for installation of the grinder pump station is in the basement of the building it will serve. However, due consideration must be given when choosing an indoor location. If there is a risk of damage to items located in the basement level, other provisions should be made during basement installation or an outdoor unit should be considered.

Considerations such as ownership of the pumps by a municipality or private organization and/or the need for outdoor accessibility frequently dictate outdoor, in-ground installations. For outdoor installations, all GP models are available with high density polyethylene (HDPE) integral accessways ranging in height up to 10 feet. By keeping the unit as close as possible to the building, the lengths of gravity sewer and wiring will be minimized, keeping installation costs lower while reducing the chances of infiltration in the gravity flow section.

AC power from the building being served should be used for the grinder pump. Separate power sources add to installation and O&M costs, decrease overall reliability and frequently represent an aesthetic issue.

When two dwellings are to be served by a single unit, the station is usually placed in a position requiring the shortest gravity drains from each home. With multi-family buildings, more than one grinder pump may be required.

Pipe Selection

The final determination of the type of pipe to be used is the responsibility of the consulting engineer. In addition, the requirements of local codes, soil, terrain, water and weather conditions that prevail will guide this decision.

Although pipe fabricated from any approved material may be used, most LPS systems have been built with PVC and HDPE pipe. Continuous coils of small-diameter, HDPE pipe can be installed with automatic trenching machines and horizontal drilling machines to sewer areas at lower cost.

Table 1 PIPE WATER CAPACITY Gallons/100 feet of Pipe Length Nominal Pipe Sch 40 **SDR 21 SDR 11** Size (in.) **HDPE PVC PVC** 7.8 9.2 7.4 1 1/4 9.9 12.1 1 1/2 10.6 2 17.4 18.8 15.4 2 1/2 23.9 27.6 40.9 33.5 3 38.4 4 55.3 66.1 67.5 5 103.1 84.5 103.7 6 150.0 146.0 119.9 8 260.0 249.0 203.2

PVC PIPE	Table 2 COMPARIS Pipe Size = 2	
Parameter	Sch 40	SDR 21
Wall Thickness, in.	0.154	0.113
Inside Diameter, in.	2.067	2.149
50 gpm Friction Loss, ft/100 ft	4.16	3.44

Table 1 compares the water capacity of two types of PVC pipe commonly used: SDR-21 and Sch 40, and one type of HDPE, SDR-11. All three have adequate pressure ratings for low pressure sewer service.

Although both types of PVC pipes are suitable, the three parameters compared in Table 2 illustrate why SDR-21 is suggested as a good compromise between capacity, strength, friction loss characteristics and cost.

System Layout

A preliminary sketch of the entire pressure sewer system should be prepared (Figure 3). Pump models should be selected and their location (elevation) should be noted. The location and direction of flow of each lateral, zone and main, and the point of discharge should be shown.

The system should be designed to give the shortest runs and the fewest abrupt changes in direction. "Loops" in the system must be avoided as they lead to unpredictable and uneven distribution of flow.

Although not shown in Figure 3, the elevation of the shutoff valve of the lowest-lying pump in each zone should be recorded and used in the final determination of static head loss. Since Environment One grinder pumps are semi-positive displacement and relatively insensitive to changes in head, precisely surveyed profiles are unnecessary.

Air/vacuum valves, air release valves and combination air valves serve to prevent the concentration of air at high points within a system. This is accomplished by exhausting large quantities of air as the system is filled and also by releasing pockets of air as they accumulate while the system is in operation and under pressure. Air/vacuum valves and combination air valves also serve to prevent a potentially destructive vacuum from forming.

Air/vacuum valves should be installed at all system high points and significant changes in grade. Combination air valves should be installed at those high points where air pockets can form. Air release valves should be installed at intervals of 2,000 to 2,500 feet on all long horizontal runs that lack a clearly defined high point.

Air relief valves should be installed at the beginning of each downward leg in the system that exhibits a 30-foot or more drop. Trapped pockets of air in the system not only add static head, but also increase friction losses by reducing the cross sectional area available for flow. Air will accumulate in downhill runs preceded by an uphill run.

Long ascending or descending lines require air and vacuum or dual-function valves placed at approximately 2000-foot intervals. Long horizontal runs require dual function valves placed at approximately 2000-foot intervals.

Pressure air release valves allow air and/or gas to continuously and automatically released from a pressurized liquid system. If air or gas pockets collect at the high points in a pumped system, then those pressurized air pockets can begin to displace usable pipe cross section. As the cross section of the pipe artificially decreases, the pump sees this situation as increased resistance to its ability to force the liquid through the pipe.

Air relief valves at high points may be necessary, depending on total system head, flow velocity and the particular profile. The engineer should consult Environment One in cases where trapped air is considered a potential problem.

Cleanout and flushing stations should be incorporated into the pipe layout. In general, cleanouts should be installed at the terminal end of each main, every 1,000 to 1,500 feet on straight runs of pipe, and whenever two or more mains come together and feed into another main.

Zone Designations

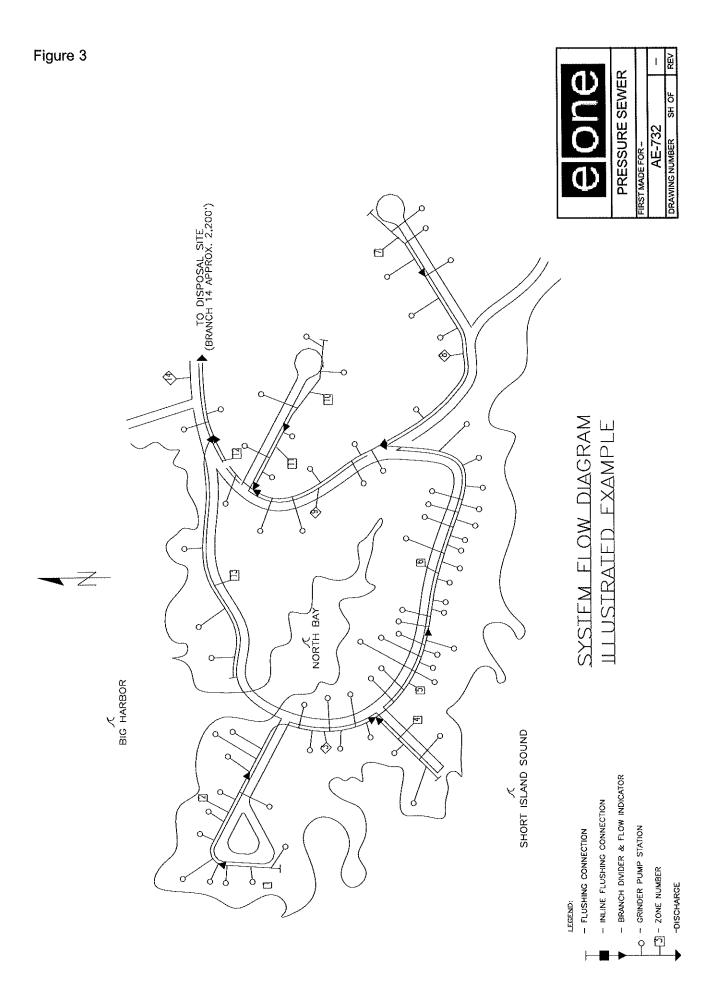
The LPS system illustrated in Figure 3 contains 72 pumps and is divided into 14 individually numbered zones. Division into zones facilitates final selection of pipe sizes, which are appropriate in relation to the requirements that flow velocity in the system is adequate and that both static and dynamic head losses are within design criteria. Assignment of individual zones follows from the relationship between the accumulating total number of pumps in a system to the predicted number that will periodically operate simultaneously (Table 3).

Table 4 was initially developed after careful analysis of more than 58,000 pump events in a 307-day period during the Albany project (4). It was extended for larger systems by application of probability theory. The validity of this table has since been confirmed by actual operating experience with thousands of large and small LPS systems during a 34-year period.

Using Figure 3, the actual exercise of assigning zones is largely mechanical. The single pump farthest from the discharge point in any main or lateral constitutes a zone. This and downstream pumps along the main are accumulated until their aggregate number is sufficient to increase the number of pumps in simultaneous operations by one, i.e., until the predicted maximum flow increases by 11 gpm.

Figure 3 shows that zones 1, 2 and 3 end when the number of pumps connected total 3, 6 and 9, and the number of pumps in daily simultaneous operation are 2, 3 and 4, respectively.

Any place where two or more sections of main join, or where the outfall is reached, also determines the end of a zone. This design rule takes precedence over the procedure stated above, as seen in



Completion of Pipe Schedule and Zone Analysis

The data recorded on the System Flow Diagram (Figure 3) is then transferred to Table 4.

Table 4 Column No.	Designation
1	Zone Number
2	Connects to Zone
3	Number of Pumps in
	Zone
4	Accumulated
	Pumps in Zone
11	Length of Main this
	Zone in Feet

Column 4 is completed by referring to Table 3, where the maximum number of pumps in simultaneous operation is given as a function of the number of pumps upstream from the end of the particular zone. The output of each zone will vary slightly with head requirements, but under typical conditions, the flow is approximately 11 gpm. Calculate the maximum anticipated flow for each zone by multiplying the number of simultaneous operations in Column 7 by 11 gpm and record the results in Column 8.

To complete columns 9, 10, 12 and 13, refer to Flow Velocity and Friction Head Loss table for the type of pipe selected — in this case, Table 5 for SDR-21. It will be seen that the engineer will frequently be presented with more than one option when selecting pipe size. Sometimes a compromise in pipe size will be required to meet present needs as well as planned future development. As a general rule, pipe sizes should be selected to minimize friction losses while keeping velocity near or above 2 feet per second.

For example, Zone 1 has a maximum of two pumps running (Column 7). Table 5 offers a choice of 1.25-inch, 1.5-inch or 2-inch pipe. 1.5-inch pipe is selected since flow velocity equals

Table 3 MAXIMUM NUMBER OF GRINDER PUMP CORES OPERATING DAILY

Number of Grinder Pump Cores Connected	Maximum Daily Number of Grinder Pump Cores Operating Simultaneously
1	1
2-3	2
4-9	3
10-18	4
19-30	5
31–50	6
51–80	7
81–113	8
114–146	9
147–179	10
180–212	11
213–245	12
246–278	13
279–311	14
312–344	15
345–377	16
378–410	17
411–443	18
444–476	19
477–509	20
510-542	21
543-575	22
576-608	23
609-641	24
642-674	25
675–707	26
708–740	27
741–773	28
774–806	29
807–839	30
840–872	31
873–905	32
906–938	33
939–971	34
972–1,004	35

BY:			DATE:			PRELIN SEWER	IMINAI SYS1	RY LOV	ELIMINARY LOW-PRESSURE IER SYSTEM PIPE SCHEDULE	SURE EDULE		EnV	Environment/One	nent	/On	(1)	
PIPE:	SDR 21 PVC	1 PVC				A	ID ZON	JE ANA	AND ZONE ANALYSIS OF:	<u>.</u>				S	CORPORATION		
PREPA	PREPARED FOR:						IIIIIctr	Illustrated Example	elume.		AE						
								Table 4	<u>}</u>		SHEET NO.	NO.		æ		REV	V
,-	2	3	4	5	9	7	8	6	10	Ŧ	12	13	14	15		17	48
ZONE	CONN.	NO.	ACCUM.	GAL/DAY	MAX.	MAX.	MAX.	PIPE SIZE (in)	MAX. VELOCITY	LENGTH OF MAIN	FRICTION	FRICTION LOSS	ACCUM. FRICTION	MAX.	PUMP	STATIC HEAD	TOTAL DYNAMIC
	ZONE	IN ZONE		CORE	PER		(md6)		(FPS)	THIS	FACTOR (ft/100 ft)	THIS	(ft)	ELEV.	ELEV.	Œ)	HEAD
1	2	3	3	700	11	2	22	1.5	3.04	205	2.15	4.41	73.41	40	01	30	103.41
2	3	9	6	200		3	33	2.0	2.92	380	1.54	5.86	00.69	40	10	30	99.00
က	5	6	18	200	11	4	4	2.0	3.89	630	2.63	16.56	63.14	40	5	35	98.14
4	5	3	3	200	11	2	22	1.5	3.04	310	2.15	8.46	53.25	40	5	35	88.25
5	9	6	30	200	11	5	55	3.0	2.24	800	09:0	4.83	46.58	40	5	35	81.58
9	6	17	47	200	11	9	99	3.0	2.69	1,000	0.85	8.46	41.75	40	5	35	76.75
7	8	3	3	200	2	2	22	1.5	3.04	175	2.15	3.77	49.56	40	5	35	84.56
∞	6	4	7	200	11	3	33	2.0	2.92	810	1.54	12.50	45.80	40	30	10	55.80
6	12	9	09	200	Ħ	7	77	3.0	3.14	520	1.12	5.85	33.30	5	91	30	63.30
10	11	3	3	200	11	2	22	1.5	3.04	230	2.15	4.95	37.03	94	10	30	67.03
==	12	3	9	200	11	3	33	2.0	2.92	300	1.54	4.63	32.08	4	2	30	62.08
12	14	1	29	200	11	7	77	3.0	3.14	240	1.12	2.70	27.45	4	2	8	57.45
13	14	3	3	200	11	2	22	1.5	3.04	985	2.15	21.19	45.94	8	5	35	80.94
14	14	2	72	200	11	7	11	3.0	3.14	2,200	1.12	24.75	24.75	9	30	9	34.75

3.04 ft/sec and friction loss equals 2.15 ft/100 ft. Since the zone is 205 feet in length (Column 11), the total friction loss (Column 13) is:

$$HF = (2.15 \text{ ft/}100 \text{ ft})(205 \text{ ft}) = 4.41 \text{ ft}$$

For Zone 14, with 72 upstream pumps, it is seen that a maximum of seven pumps can be running simultaneously. Table 5 provides options of:

or

The smaller-diameter 3-inch pipe is selected because of the increased velocities, especially with the TDH below 185 feet. A choice of 3-inch pipe would lead to a friction loss in this zone of:

$$HF = (1.12 \text{ ft/}100 \text{ ft}) (2200 \text{ ft}) = 24.75 \text{ ft}$$

Accumulated friction loss (Column 14) for each zone is next determined by adding the friction loss for each zone from the system outfall (Zone 14) to the zone in question. Thus, from Figure 3 it is seen that the accumulated friction loss for Zone 1 is:

Zone Number	Friction Loss (ft)
14	24.75
12	2.70
9	5.85
6	8.46
5	4.83
3	16.56
2	5.86
1	4.41

73.41 ft = Accumulated friction loss, Zone 1

The same summation is completed for each zone.

To complete the hydraulic analysis, refer to the drawing contours and record in Column 15 the maximum line elevation between the point of discharge and the zone under consideration. In Column 16, record the elevation of the lowest pump in the zone. Subtract the values in Column 16 from

those in Column 15 and record only positive elevation differentials in Column 17. Add the values in Column 14 to those in Column 17 and record the total in Column 18 to show the maximum combination of friction and static head a pump will experience at any given point in the system.

Review

The accumulated data in Table 4 should finally be reviewed for conformity with the criteria of flow velocity greater than or equal to 2.0 ft/sec and total design head less than or equal to 185 feet. If the system pressure exceeds 92 feet, the number of cores operating will remain the same and the flow from each pump will be reduced from 11 gpm to 9 gpm.

Data should be reviewed to determine whether system improvements could result from construction modifications. As an example, deeper burial of pipe in one or two critical high-elevation zones might bring the entire system into compliance with design criteria. Environment One should be consulted in marginal cases and/or concerning:

- · Odor control issues
- Frost protection issues
- Excessive static head conditions
- Excessive total dynamic head conditions
- Unusual applications

Table 5 SDR 21 PVC PIPE

Flow Velocity and Friction Head Loss vs Pumps in Simultaneous Operation (C = 150)

	1 1/	'4 in.	1 1/	'2 in.	2	in.	2 1/	/2 in.	3	in.	4	in.	5	in.	6	in.	8	in.	
N	V	H _F	٧	H _F	V	H _F	٧	H _F	٧	H _F	٧	H _F	V	H _F	V	H _F	V	H _F	N
1	1.99	1.15	1.52	0.60				,		·		•		·		•		·	1
2	3.99	4.16	3.04	2.15	1.95 2.92	0.73	4 00	0.64											2
3 4	5.98 7.97	8.82 15.02	4.56 6.08	4.56 7.77	3.89	1.54 2.63	1.99 2.66	0.61 1.04	1.79	0.40									3 4
5	7,07	10.02	0.00		4.87	3.97	3.32	1.57	2.24	0.60									5
6					5.84	5.57	3.99	2.20	2.69	0.85									6
7					6.81	7.41	4.65	2.93	3.14	1.12	1.90	0.33							7
8							5.32	3.75	3.59	1.44	2.17	0.42							8
9 10							5.98 6.64	4.66 5.67	4.04 4.49	1.79 2.18	2.44 2.71	0.53 0.64							9
11							0.04	3.07	4.93	2.60	2.98	0.76	1.95	0.27					11
12									5.38	3.05	3.25	0.90	2.13	0.32					12
13]		5.83	3.54	3.52	1.04	2.31	0.37					13
14									6.28	4.06	3.80	1.19	2.48	0.43	4 00	0.04			14
15 16											4.07 4.34	1.36 1.53	2.66 2.84	0.48 0.55	1.88 2.00	0.21			15 16
17											4.61	1.71	3.02	0.61	2.13	0.26			17
18											4.88	1.90	3.19	0.68	2.25	0.29			18
19											5.15	2.10	3.37	0.75	2.38	0.32			19
20 21											5.42	2.31	3.55	0.82	2.50	0.35			20
22											5.69 5.96	2.53 2.76	3.73	0.90 0.98	2.63 2.75	0.39 0.42			21 22
23											6.24	2.99	4.08	1.07		0.46			23
24		Head Loss Calculations											4.26	1.16	3.00	0.49			24
25 26		From Modified Hazen - Williams Formula —											4.44	1.25	3.13	0.53			25
26													4.61 4.79	1.34 1.44	3.25 3.38	0.57 0.61	1.99	0.17	26 27
28		$H_F = .2083 \left[\left(\frac{100}{C} \right)^{1.852} \times \frac{q^{1.852}}{d^{4.8655}} \right]$											4.73	1.54	3.50	0.66	2.07	0.17	28
29						u							5.15	1.64	3.63	0.70	2.14	0.19	29
30		_ V = .	.3208	$\frac{\mathbf{q}}{\mathbf{q}}$									5.32	1.75	3.75	0.75	2.21	0.21	30
31				А									5.50	1.86	3.88	0.79	2.29	0.22	31
32 33		Δ=	$d^2\pi$	= cros	e-eart	ional fl	UM SU	ı in					5.68 5.86	1.97 2.08	4.01 4.13	0.84 0.89	2.36 2.44	0.23 0.25	32
34		7-	4	- 6103	3-3601	ioriai ii	OW, SC	f. 11 t.					6.03	2.20	4.26	0.94	2.51	0.26	34
35		_c=	150										6.21	2.32	4.38	0.99	2.58	0.28	35
36		q = 1	flow in	gallor	is per	minute)								4.51	1.05	2.66	0.29	36
37 38				pipe ir											4.63 4.76	1.10 1.16	2.73 2.81	0.30	
39		[a	verage	e O.D.	- (2 x	min. w	all thic	kness]						4.76	ŧ	2.88	0.34	
40			ı	I	ı	1	1	l	I						5.01	į.	2.95	0.35	
41															5.13	1.33	3.03	0.37	41
42															5.26		3.10	0.39	42
43 44		***************************************													5.38	1.45		0.40	1 1
44		La constitución de la constituci										-			5.51 5.63	1.52 1.58		0.42 0.44	1 1
46	1	N=N	i Vumbe	ı er of pu	ımns d	perati	ng at	11 ann	1 1				<u> </u>		5.76	1.65	3.40	0.46	
47				elocity				96"	•						5.88	1.72	3.47	0.47	47
48				n head			0 ft of	pipe							6.01			0.49	
49 50		•	1	1	1	 I	1	 I	1						6.13	1.85		0.51	
30	<u> </u>	<u> </u>	I	ł	<u></u>	L	<u></u>	<u></u>	L	L	1	<u> </u>	<u> </u>	<u> </u>	6.26	1.92	3.69	0.53	1 20

Table 6 SCHEDULE 40 PVC PIPE

Flow Velocity and Friction Head Loss vs Pumps in Simultaneous Operation (C = 150)

	1 1/	4 in.	1 1/	⁄2 in.	2	in.	2 1/	'2 in.	3	ìn.	4	in.	5	in.	6	in.	8	in.	
N	٧	H _F	٧	H _F	V	H _F	٧	H_{F}	V	H _F	N								
1	2.36	1.74	1.73	0.82	1.05	0.24						Î						•	1
3	4.72	6.28	3.47 5.20	2.97	2.10 3.15	0.88 1.86	1.47	0.37			1								2
4	7.08	13.31	6.93	6.29 10.71	4.21	3.18	2.21 2.95	0.79 1.34	1.91	0.46									3 4
5			0.00	10.11	5.26	4.80	3.68		2.39	0.70									5
6					6.31	6.73	4.42	2.83	2.87	0.99		,							6
7							5.16	3.77	3.34	1.31	1.94	0.35							7
8			•				5.89	4.83	3.82	1.68	2.22	0.45							8
9							6.63	6.01	4.30 4.78	2.09 2.54	2.49 2.77	0.56 0.68							9 10
11									5.25	3.03	3.05	0.81	1.94	0.27					11
12									5.73	3.56	3.33	0.95	2.12	0.32					12
13									6.21	4.13	3.60	1.10	2.29	0.37					13
14 15											3.88	1.26	2.47	0.42					14
16											4.16 4.44	1.43 1.62	2.65 2.82	0.48 0.54	1.95	0.22			15 16
17											4.71	1.81	3.00	0.60	2.08	0.25			17
18											4.99	2.01	3.17	0.67	2.20	0.27			18
19			1								5.27	2.22	3.35	0.74	2.32	0.30			19
20 21											5.54 5.82	2.44 2.67	3.53 3.70	0.81	2.44 2.56	0.33			20
22											6.10	2.91	3.88	0.89	2.69	0.36 0.40			21 22
23											****		4.06	1.05	2.81	0.43			23
24		Hea	d Los	s Calc	ulatio	ns	•	•			Ì		4.23	1.14	2.93	0.47			24
25		_ Fror	n Mod	dified I	Hazen	- Will	iams	Formu	ıla				4.41	1.23	3.05	0.50			25
26 27				r 100	1.852	a 1.852	٦						4.59 4.76	1.32 1.42	3.17 3.30	0.54 0.58			26 27
28		H _F =	.2083	$3\left[\left(\frac{100}{C}\right)\right]$) x	d ^{4.8655}	J						4.94	1.52	3.42	0.62	1.98	0.16	28
29						u							5.11		3.54	0.66	2.05	0.17	29
30		V = .	.3208	4									5.29	1.72	3.66	0.70	2.12	0.19	30
31				^									5.47	1.83	3.79	0.75	2.19	0.20	31
32 33		A =	$d^2\pi$	= cros	s-sect	ional fl	ow. so	ı. in.					5.64 5.82	1.94 2.06	3.91 4.03	0.79 0.84	2.26 2.33	0.21 0.22	32 33
34		' '	4				,	1					6.00	2.17	4.15	0.89	2.40	0.23	34
35		_ C =	150										6.17		4.27	0.94	2.47	0.25	35
36 37				ı gallor)								4.40	0.99		0.26	36
38]			pipe ir					_						4.52 4.64	1.04 1.09	2.61	0.27 0.29	38
39		[a	verag	e O.D.	- (2 x	min. w	all thic	ckness	.]						4.76	1.15	2.75		39
40			I	1	I		1	1	I						4.88	1.20	2.82		40
41															5.01	1.26	2.89	0.33	41
42															5.13	1.31	2.96		42
43															5.25	1.37	3.03	0.36	43
45															5.37 5.49	1.43 1.49	3.11 3.18		44 45
46		N = 1	lumb	er of pu	admi.	perati	ng at	11 apn	 n						5.62	1.56	3.25		46
47				elocity				יישט יי	-						5.74	1.62	3.32	0.43	47
48				on head			00 ft of	pipe			1				5.86	1.68	3.39		48
49 50		-	1	I	1	I	ı	, <i>,</i> I	ı						5.98	1.75	3.46		49
100	<u> </u>	<u>i</u>	1	<u> </u>	<u> </u>	L	L	L	<u> </u>		<u> </u>	<u> </u>	I	l	6.11	1.81	3.53	0.48	50

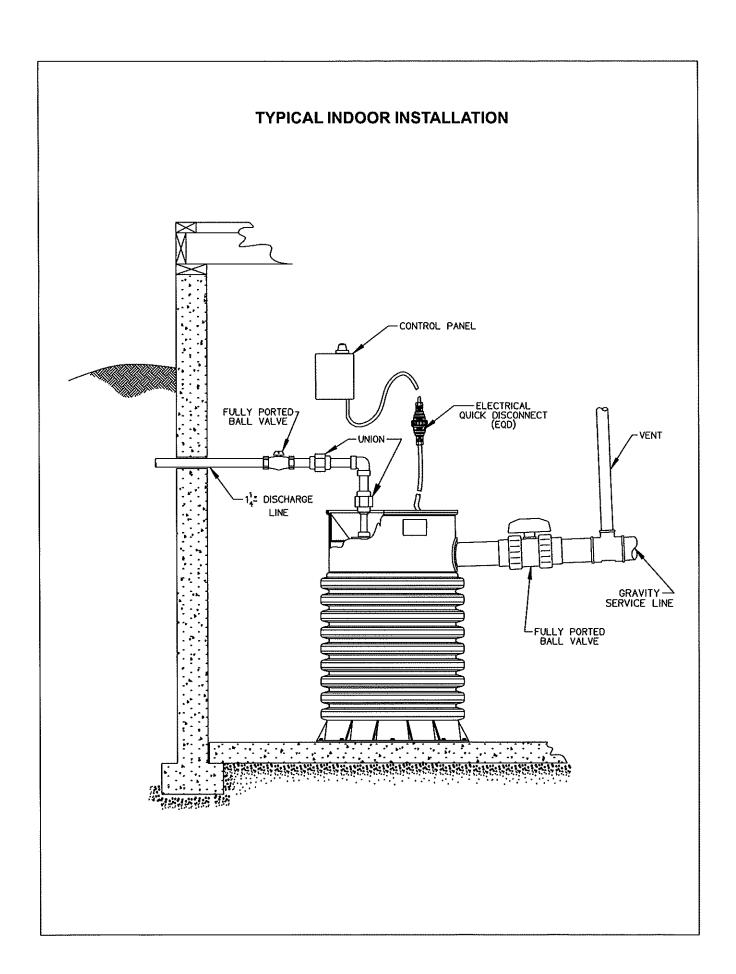
Table 7 SDR 11 HDPE PIPE

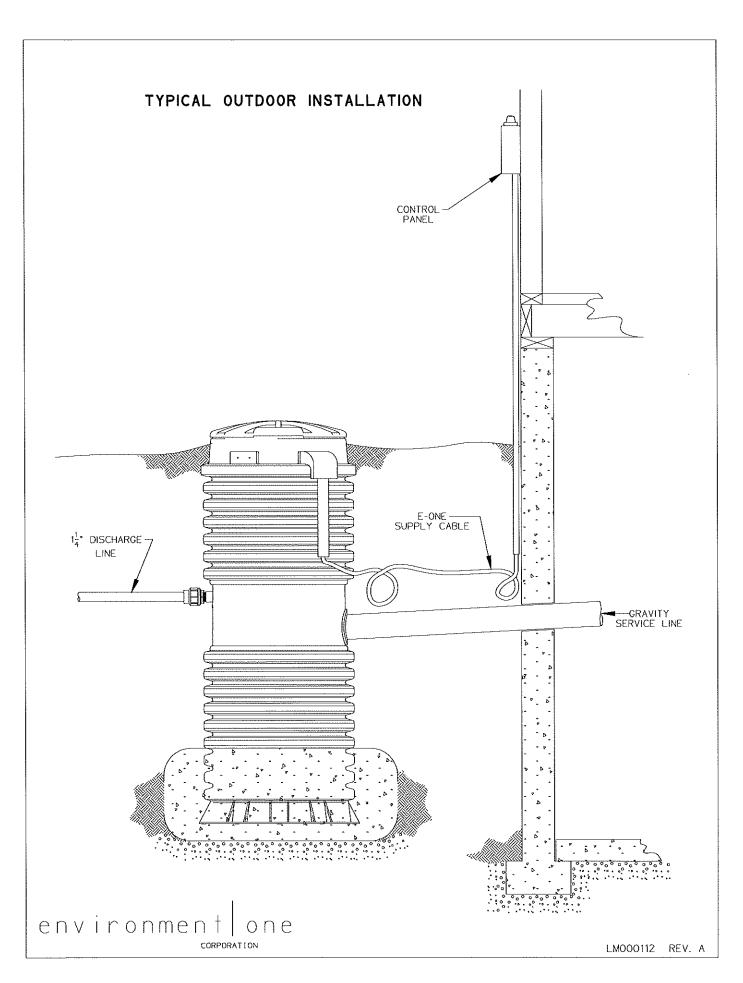
Flow Velocity and Friction Head Loss vs Pumps in Simultaneous Operation (C = 155)

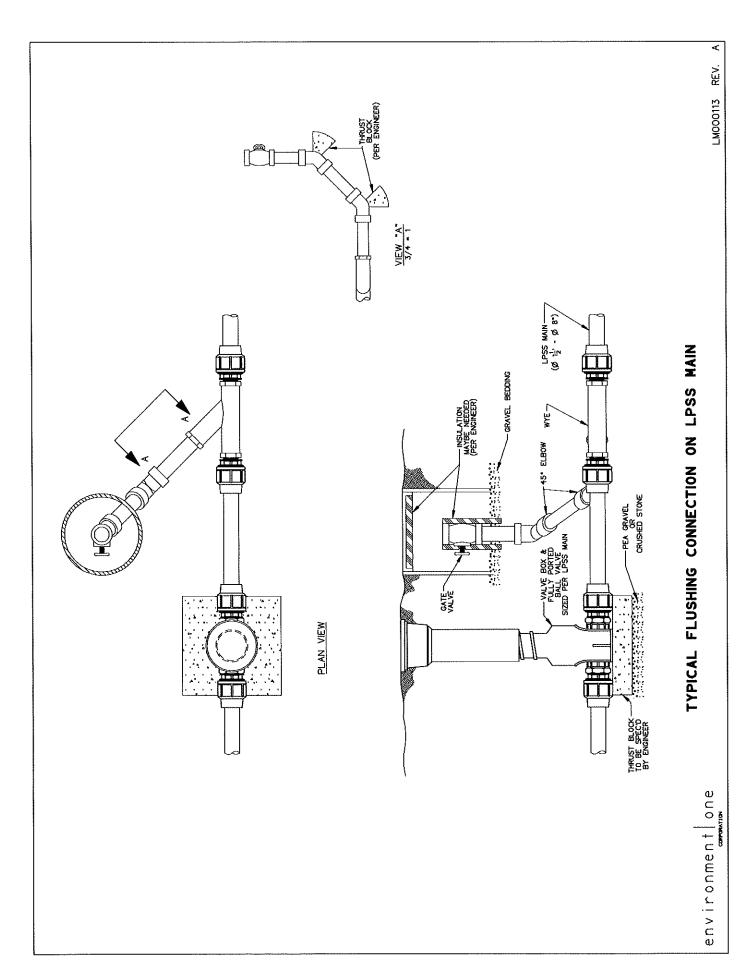
	1 1/	⁄4 in.	1 1/	'2 in.	2	in.	3	in.	4	in.	5	in.	6	n.	8 i	n.	
N	٧	H _F	V	H _F	V	H _F	٧	H _F	V	H _F	V	H _F	٧	H _F	٧	H _F	N
1	2.47	1.84	1.86	0.92	0.00												1
3	4.95 7.42	6.63 14.04	3.72 5.58	3.32 7.03	2.38 3.57	1.12 2.37	1.64	0.36									2 3
4	1.72	1 1 1 0 1	7.44	11.98	4.76	4.04	2.19	0.61									4
5					5.95	6.11	2.74	0.92									5
6					7.14	8.56	3.29	1.30	1.99	0.38							6
7 8							3.83	1.72	2.32	0.51 0.65							7
9							4.38 4.93	2.21 2.75	2.65 2.98	0.83	1.95	0.29					8 9
10							5.48	3.34	3.31	0.98	2.17	0.35					10
11							6.03	3.98	3.65	1.17	2.39	0.42					11
12									3.98	1.38	2.60	0.49	4 00				12
13 14			1						4.31 4.64	1.60 1.83	2.82 3.04	0.57 0.65	1.99 2.14	0.24 0.28			13 14
15									4.97	2.08	3.25	0.74	2.29	0.32			15
16									5.30	2.35	3.47	0.84	2.45	0.36			16
17									5.63	2.63	3.69	0.94	2.60	0.40			17
18 19									5.97	2.92	3.90	1.04	2.75	0.44			18
20									6.30	3.23	4.12 4.34	1.15 1.27	2.90 3.06	0.49 0.54			19 20
21											4.56	1.39	3.21	0.59			21
22											4.77 4.99	1.51	3.36	0.64	1.98	0.18	22
23		Head Loss Calculations										1.64	3.52	0.70	2.08	0.19	23
24 25		Head Loss Calculations										1.77 1.91	3.67 3.82	0.76 0.82	2.17 2.26	0.21 0.23	24 25
26		From Modified Hazen - Williams Formula —										2.06	3.98	0.82	2.35	0.23	26
27		$H_F = .2083 \left[\left(\frac{100}{C} \right)^{1.852} \times \frac{q^{1.852}}{d^{4.8655}} \right]$										2.21	4.13	0.94	2.44	0.26	27
28		' 'F	.2000	, r, C	^	d ^{4.865} 5	J				6.07	2.36	4.28	1.01	2.53	0.28	28
29 30		\ \/	2200	q									4.43	1.08	2.62	0.30	29
31		+ v = ·	.3208	Ā									4.59 4.74	1.15 1.22	2.71 2.80	0.32 0.34	30 31
32			d2m										4.89	1.29	2.89	0.36	32
33		A =	$\frac{d \kappa}{d}$	= cros	s-sect	ional fl	ow, sc	ı. in.					5.05	1.37	2.98	0.38	33
34 35		C -	150								1		5.20	1.44	3.07	0.40	34
36		C =		gallon	e nar	minute							5.35 5.50	1.52 1.60	3.16 3.25	0.42 0.44	35 36
37				pipe ir			•						5.66		3.34	0.47	37
38				e O.D.			all thin	kness	1				5.81	1.77	3.43	0.49	38
39		"	~g\		,,		1		<i>3</i> 1	1			5.96	1.86	3.52	0.52	39
40 41												<u> </u>	6.12	1.95	3.61 3.70	0.54 0.57	40
42															3.70	0.57	41
43												Į			3.88	0.62	43
44													1		3.97	0.65	44
45 46		 	<u> </u>	L	<u> </u>		ļ			ļ					4.06	0.67	45
47				er of pu			ng at	11 gpn	n						4.15 4.24	0.70 0.73	46 47
48				elocity)() # ~4	nina							4.33	0.76	48
49		□ ^e ==	THEUC	on head	. 1088	111 IV 19	JU IE OI	pipe							4.42	0.79	49
50					<u> </u>		<u> </u>	<u> </u>			<u>L. </u>	<u> </u>	<u> </u>		4.51	0.82	50

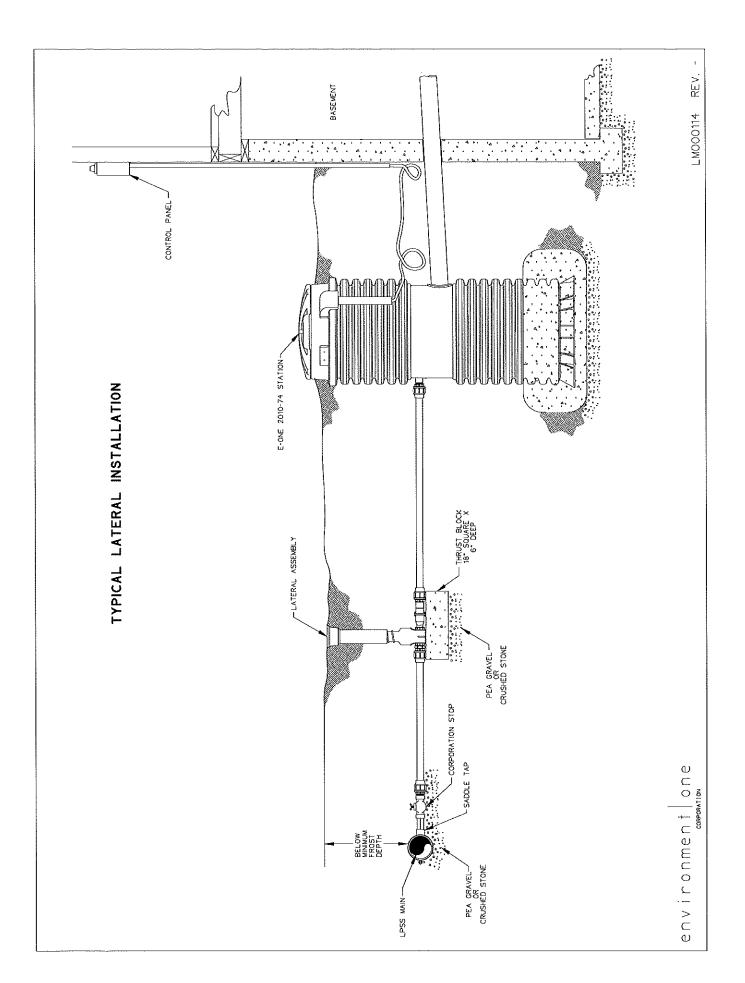
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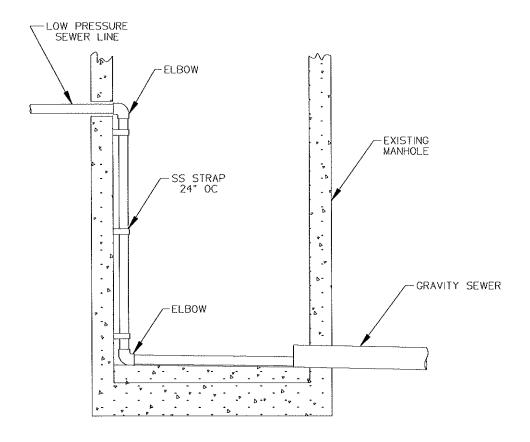






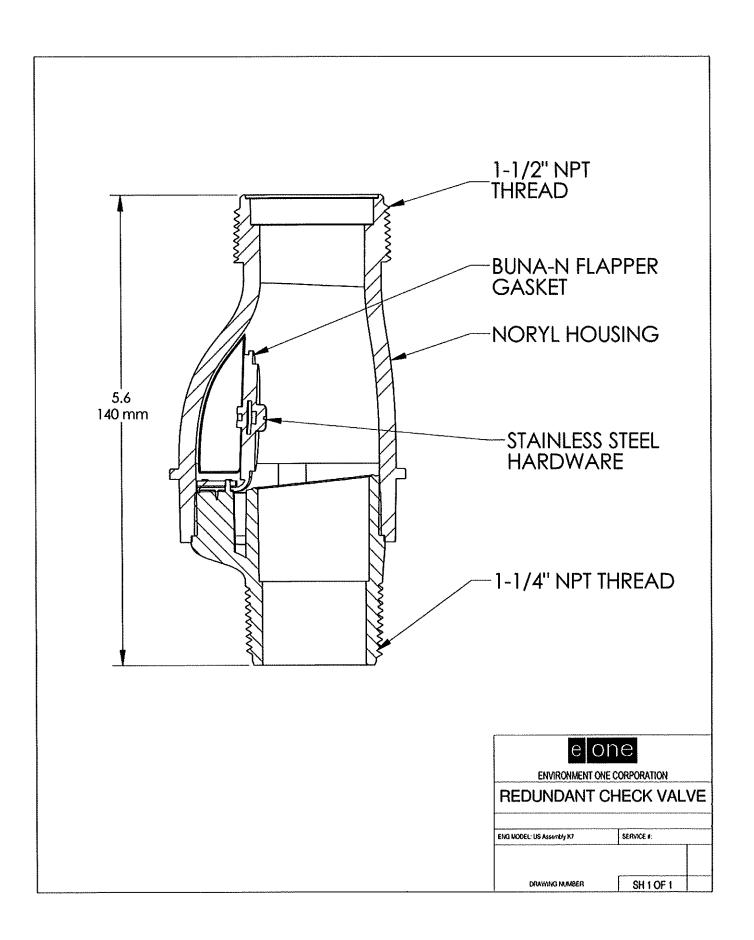


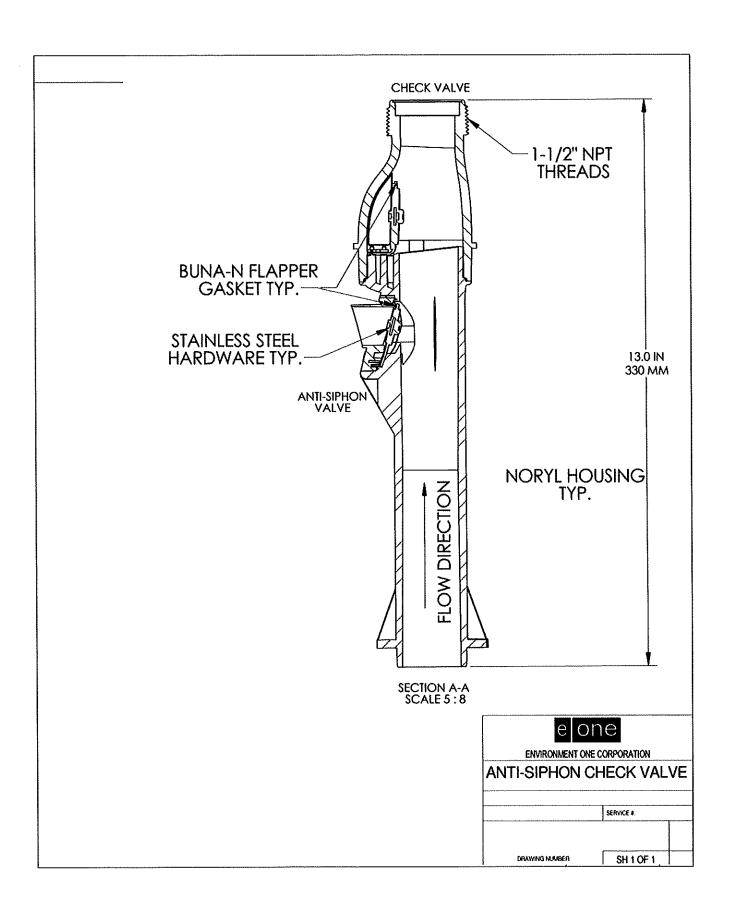
TYPICAL DROP CONNECTION LPSS IN EXISTING MANHOLE



environment one

LM000115 REV. -





Manufacturer Evaluation List

Service and Maintenance Check List

General Requirements for Low Pressure Sewer Systems

- Local fast-response service and maintenance organization has been designated
- Manufacturers of all equipment specified for the system have supplied all installation details
- Warranties for all equipment specified for the system have been evaluated
- Fast replacement parts availability for all equipment in the system has been ensured by each equipment manufacturer
- User instructions have been supplied to homeowners

Grinder Pump

- Designated for the specific purpose of grinding and pumping domestic wastewater
- Suitable for parallel operation in a system containing thousands of pumps connected to a common discharge line
- · Has a history of reliable operation
- Compatible with existing power sources and provides economical operation
- Simple to service and troubleshoot, easily accessible for removal of grinder pump core; designed with simple wiring and controls; easily disassembled and reassembled
- Warranty covering parts and labor for a reasonable length of time
- Supported by a thoroughly detailed installation manual, service manual and facilities for service training

Certifications

- Canadian Standards Association
- · Underwriters Laboratories, Inc.
- National Sanitation Foundation

Required Features

- Non-clogging pump
- Non-jamming grinder
- Anti-siphon valve integral with grinder pump
- All valves of non-clogging design: integral check valve, anti-siphon valve and redundant check valve
- High-level warning alarm

Motor

- Low rpm (1,725)
- Overload protection, built-in, automatic reset
- High torque, low starting current

Tank

- Self scouring
- Completely sealed
- Non-corroding material

Level Sensing Control

- Non-fouling type
- No moving parts in contact with sewage

Motor Controls

- Completely protected
- · Simple to service or replace
- UL-listed alarm panel



A Precision Castparts Company

Environment One Corporation 2773 Balltown Road Niskayuna, New York USA 12309–1090

Voice: (01) 518.346.6161

Fax: 518.346.6188

www.eone.com LM000353 Rev. A 060208



WH483/WR483



The model WH483 or WR483 grinder pump station is a complete unit that includes: three grinder pumps, check valve, polyethylene tank, controls, and alarm panel. Designed for higher flow applications where local codes dictate higher storage requirements. The lower portion of the tank has a smaller diameter, tapered down to a dish-shaped bottom. The large tank access opening easily accommodates installation of the grinder pumps and equipment.

- Rated for flows of 5000 gpd (18,927 lpd)
- 486 gallons (1840 liters) of capacity
- · Standard outdoor heights range from 75 inches to 122 inches

The WH483 is the "hardwired," or "wired," model where a cable connects the motor controls to the level controls through watertight penetrations.

The WR483 is the "radio frequency identification" (RFID), or "wireless," model that uses wireless technology to communicate between the level controls and the motor controls.

Operational Information

Motor

1 hp, 1,725 rpm, high torque, capacitor start, thermally protected, 120/240V, 60 Hz, 1 phase

Inlet Connections

4-inch inlet grommet standard for DWV pipe. Other inlet configurations available from the factory.

Discharge Connections

Pump discharge terminates in 1.25-inch NPT female thread. Can easily be adapted to 1.25-inch PVC pipe or any other material required by local codes.

Discharge

15 gpm at 0 psig (0.95 lps at 0 m)

11 gpm at 40 psig (0.69 lps at 28 m)

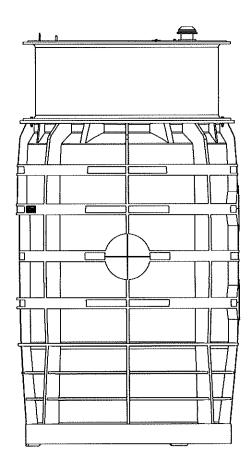
7.8 gpm at 80 psig (0.49 lps at 56 m)

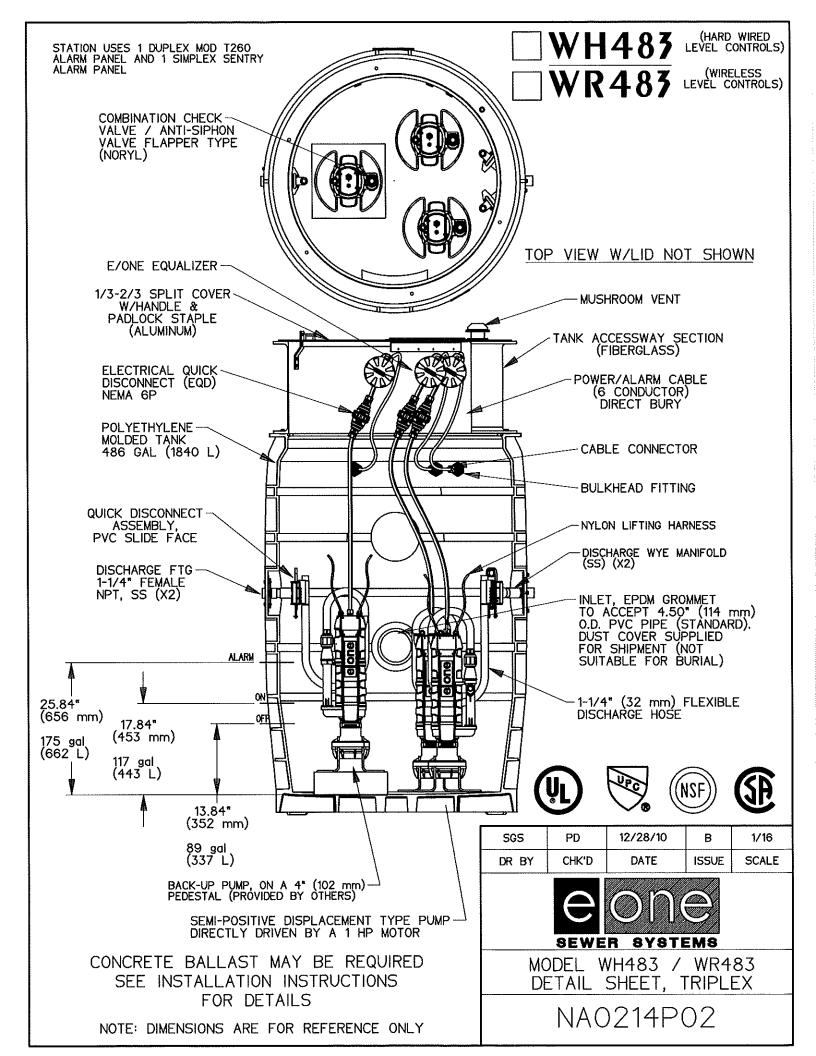
Accessories

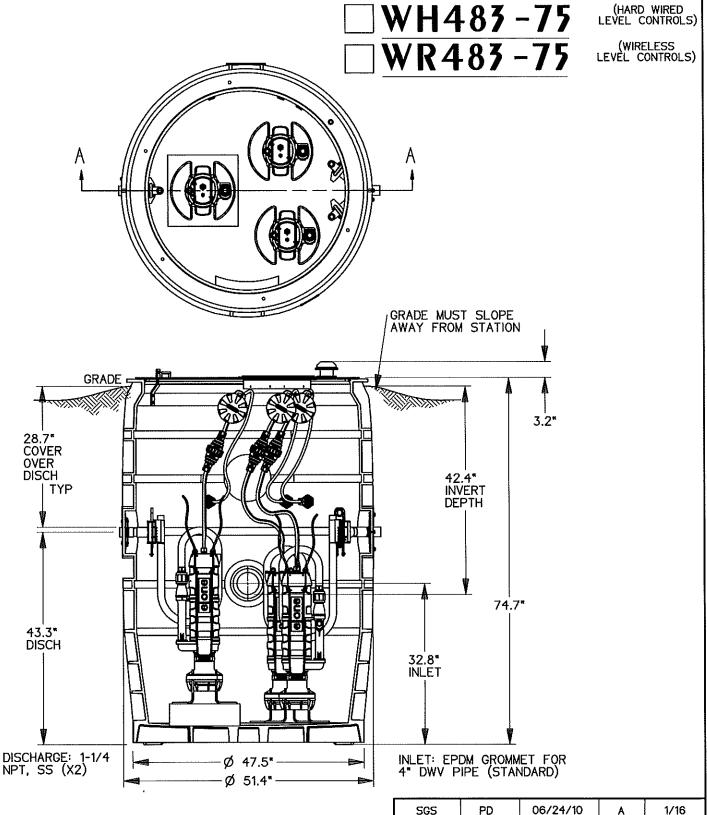
E/One requires that the Uni-Lateral, E/One's own stainless steel check valve, be installed between the grinder pump station and the street main for added protection against backflow.

Alarm panels are available with a variety of options, from basic monitoring to advanced notice of service requirements.

The Remote Sentry is ideal for installations where the alarm panel may be hidden from view.







CONCRETE BALLAST MAY BE REQUIRED SEE INSTALLATION INSTRUCTIONS FOR DETAILS

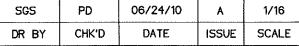
NOTE: DIMENSIONS ARE FOR REFERENCE ONLY







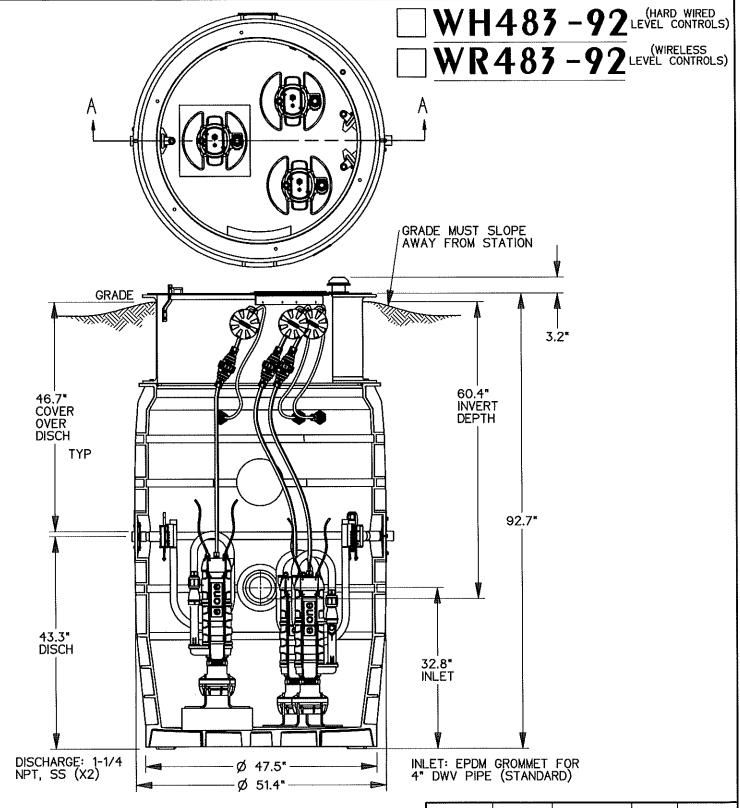






MODEL WH483-75 / WR483-75

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CONCRETE BALLAST MAY BE REQUIRED SEE INSTALLATION INSTRUCTIONS FOR DETAILS

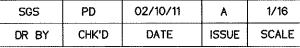
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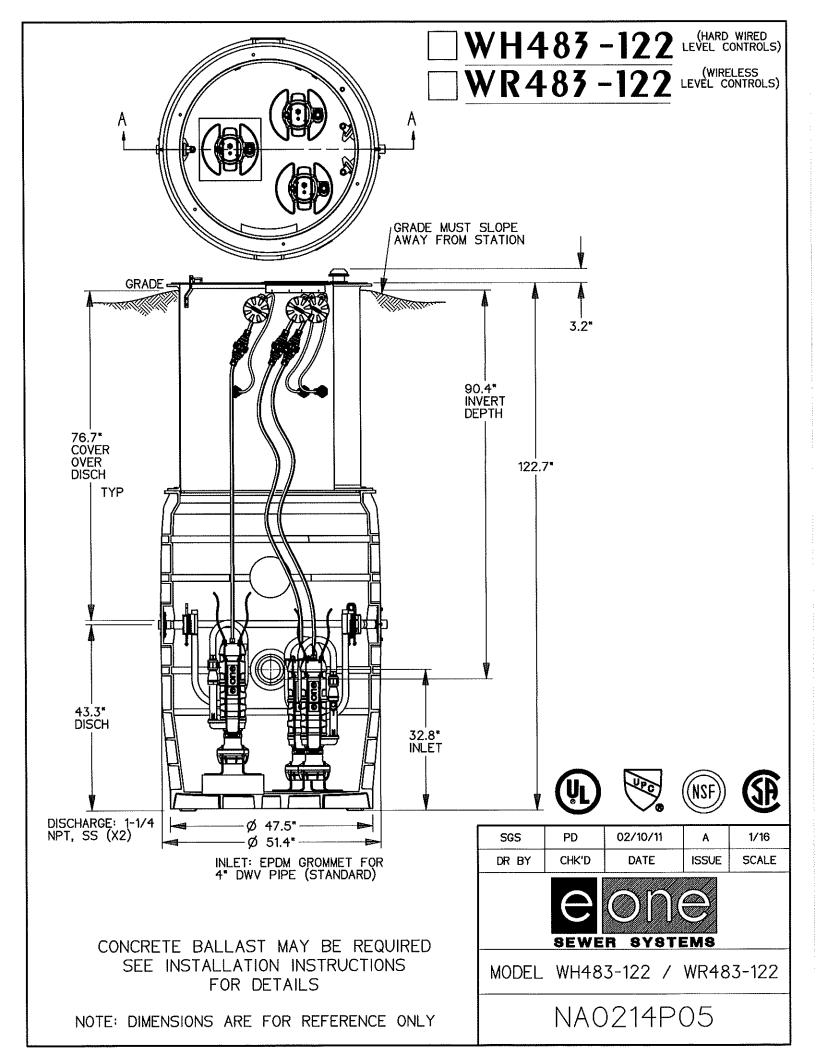


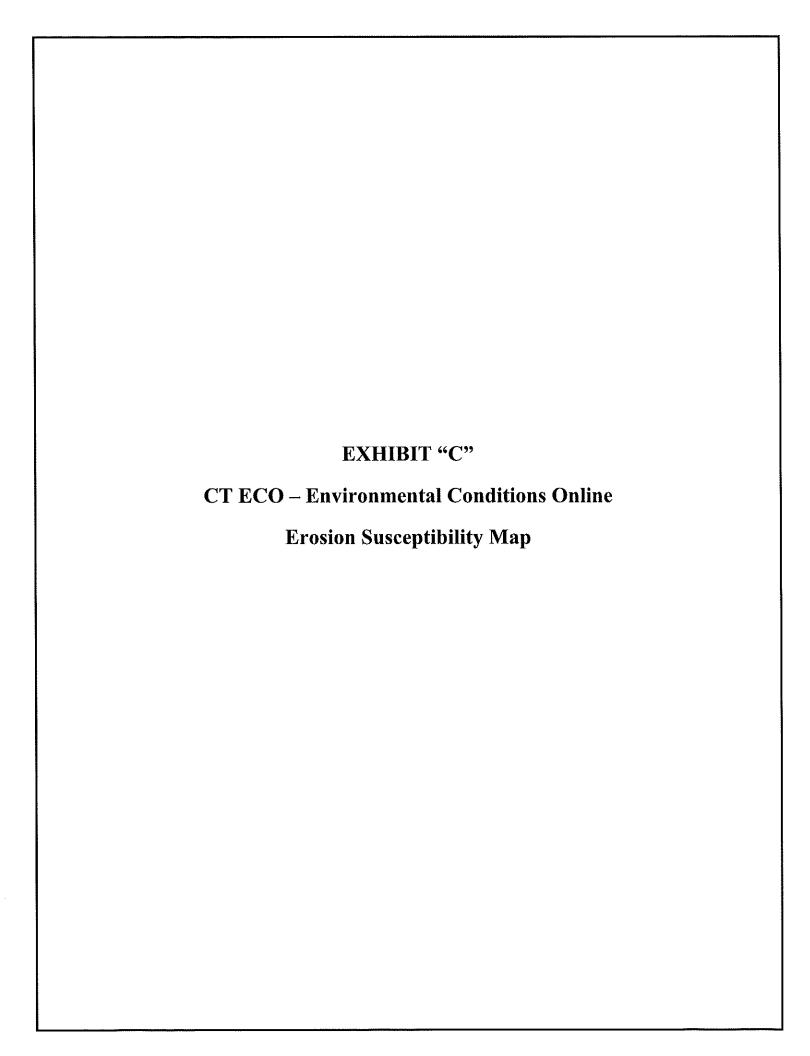


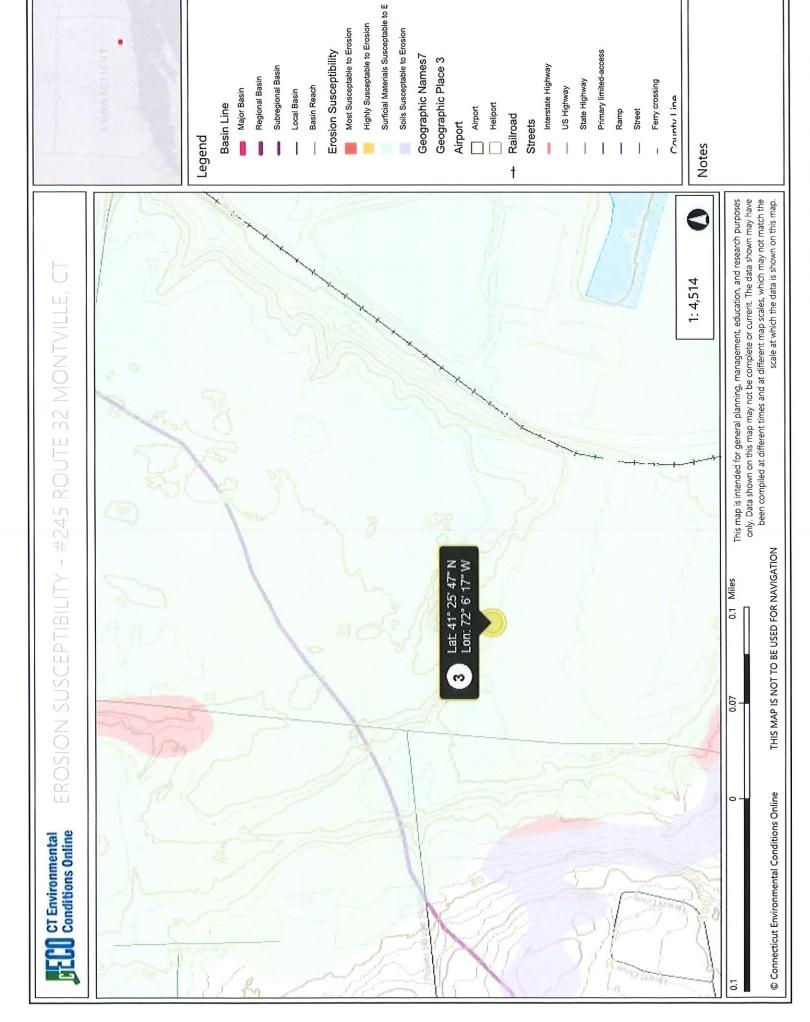


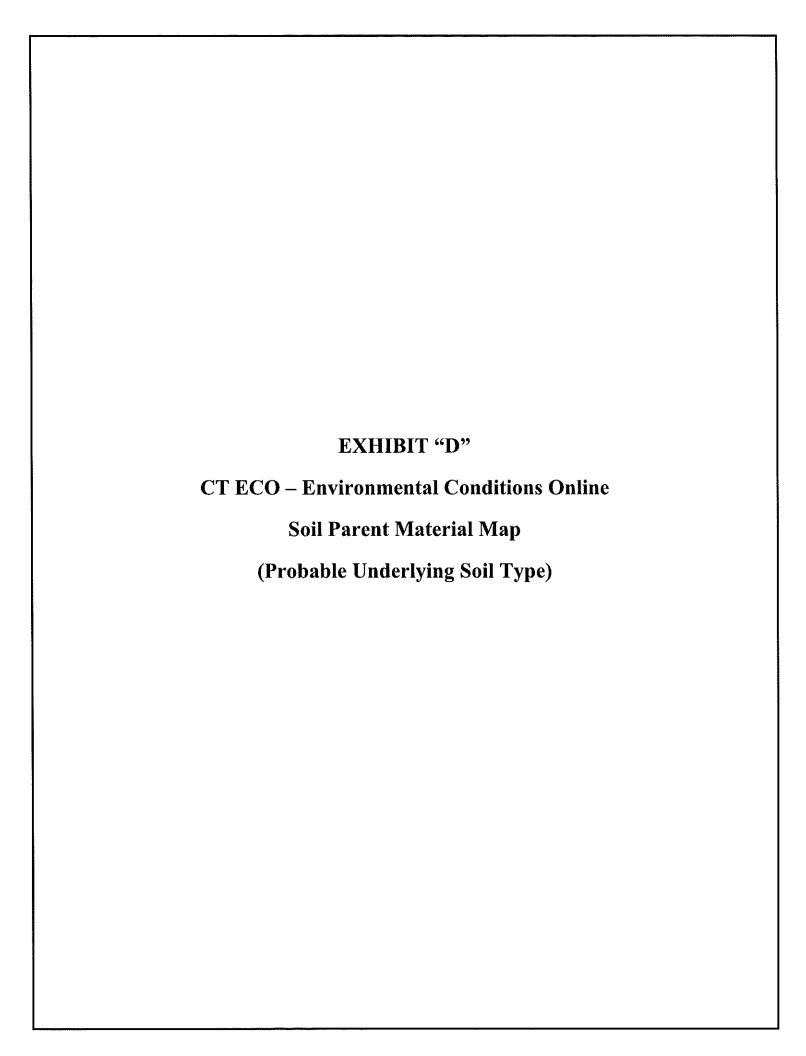
MODEL WH483-92 / WR483-92

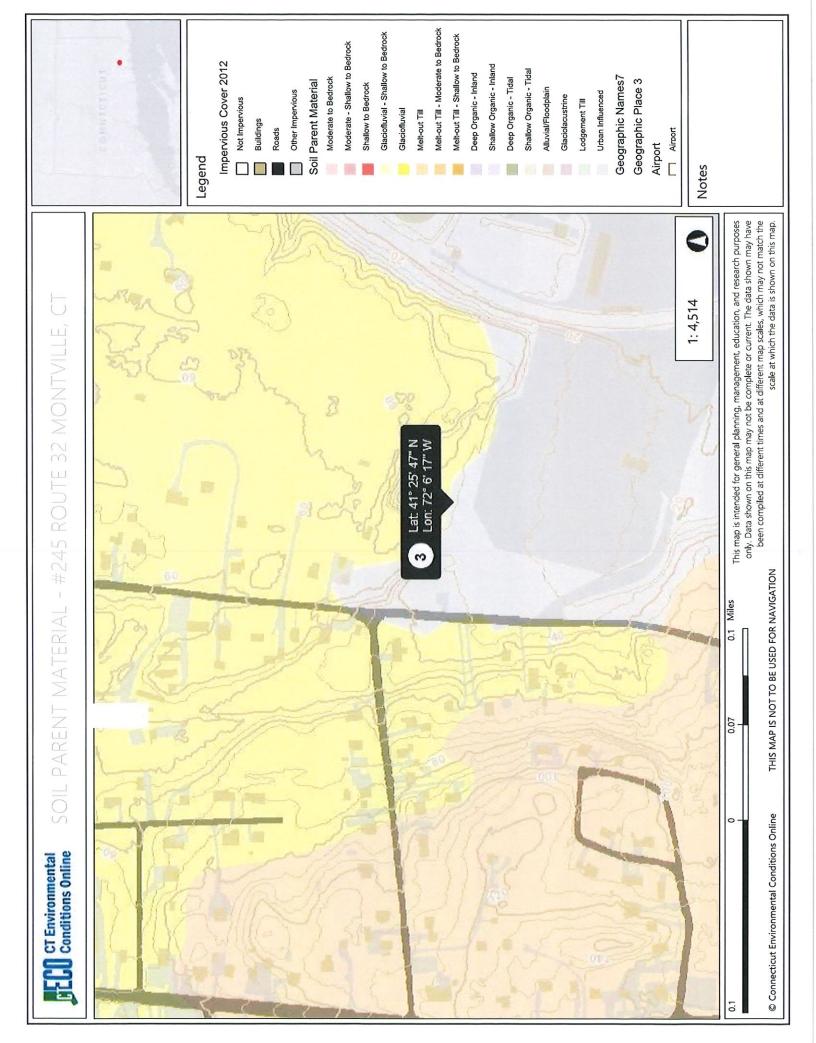
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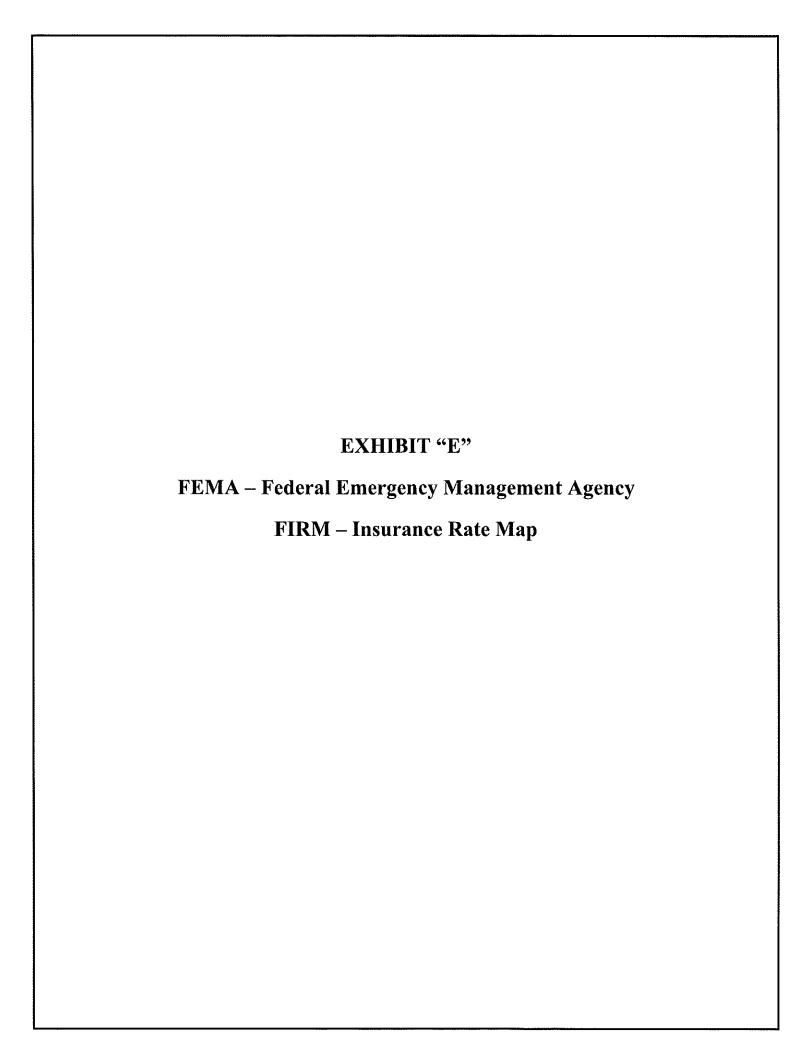






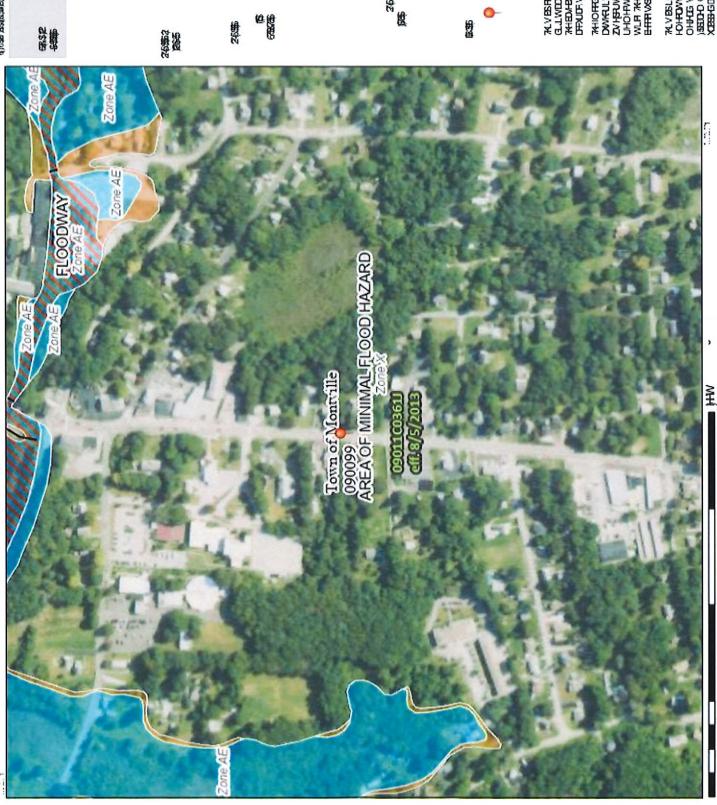




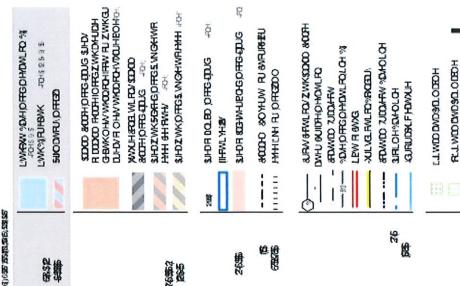


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THIS OG VSDGROWHIBLY DOGLILLEWH SLOV NOHWIGEWHIMU DEGRYGW UP DDWIRLIWDM, YHSJBUMORDWLFD

SHACE

R.V.B.HEDLH/ZWKBVWIDEDIG/IRU WHYAHR G.LWID IOHGEB/LILW LV CRV YR.GD/GARULBGEOFZ RHED/ESWEDHEDLH/ZWKBVED/ES DFAUF/WIDEJUG/ #HOFFIGURE IN THE VENT HER OFFICE OF WOUTHWIND DWARL WORL MAKE WAY THE MAKE WE THE WAY THE MAKE WAY THE MAY THE MAKE WAY THE MAY THE MAKE WAY WAY THE MAY WANT WHICH THE WAY WANT WAS THE WAY THE WAY WAS THE WAY WAS THE WAS

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